

# Optimizing Biorefineries

Austrian Stakeholder Workshop of IEA  
Bioenergy Task 42 “Biorefining”

Anton Friedl  
24.10.2013

- Downstream Processing in Biorefineries
  - „Lignozellulose Biorefinery“ (Wood and Straw)
    - Pretreatment
    - Separation processes
    - Membrane processes
- Process Optimization by Process Simulation
  - Mass- and Energy Balance
  - Exergy Analyses
  - Heat Integration (Pinch, HEN)
- Summery

- Upstream (e.g. Biomass collection)
- Pretreatment reactor
- Solid-liquid separation
- Washing (multistage)
- Concentration (e.g. membranes)
- Product purification
- Solvent recovery
- Concentrating liquid stream (MSEvap)
- By-product treatment

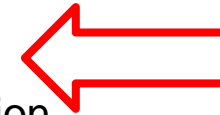
- Cellulose, Hemicellulose, Lignin, others
  - Cellulose: Polymer von  $\beta$ -(1-4)-Glucose (C6)
  - Hemicellulose: Polymer of various C5 and C6 sugars
  - Acetic acid
  - Lignin: Phenolic Polymer
  - Ash
  - „Extractives“



- Mechanical size reduction
- Physical-chemical pretreatment
  - Hydrothermal (hot water treatment)
  - „Steam Explosion“(SO<sub>2</sub>, H<sub>2</sub>SO<sub>4</sub>, Organic Acids, CO<sub>2</sub>,...)
  - Diluted acid treatment
  - Caustic treatment (lime, NaOH, NH<sub>3</sub> (Ammonia fiber explosion AFEX))
  - CO<sub>2</sub> explosion
- Chemical pretreatment
  - Oxidation (O<sub>2</sub>, O<sub>3</sub>)
  - Sulfit (SPORL)- oder Sulfat (Kraft)- cooking
  - Organosolv
    - Alcell process (APR Prozess): countercurrent extraction using ethanol (60%) („Lignol“ delignification process)
    - Organocell process (MD Prozess): Methanol (50%) / NaOH
  - Ionic liquids
- Biological treatment (fungi)

## Research Topics

- Mechanical size reduction
- Physical-chemical pretreatment
  - Hydrothermal (hot water treatment)
  - „Steam Explosion“(SO<sub>2</sub>, H<sub>2</sub>SO<sub>4</sub>, Organic Acids, CO<sub>2</sub>,...)
  - Diluted acid treatment
  - Caustic treatment (lime, NaOH, NH<sub>3</sub> (Ammonia fiber explosion AFEX))
  - CO<sub>2</sub> explosion
- Chemical pretreatment
  - Oxidation (O<sub>2</sub>, O<sub>3</sub>)
  - Sulfit (SPORL)- oder Sulfat (Kraft)- cooking
  - Organosolv
    - Alcell process (APR Prozess): countercurrent extraction using ethanol (60%) („Lignol“ delignification process)
    - Organocell process (MD Prozess): Methanol (50%) / NaOH
  - Ionic liquids
- Biological treatment (fungi)



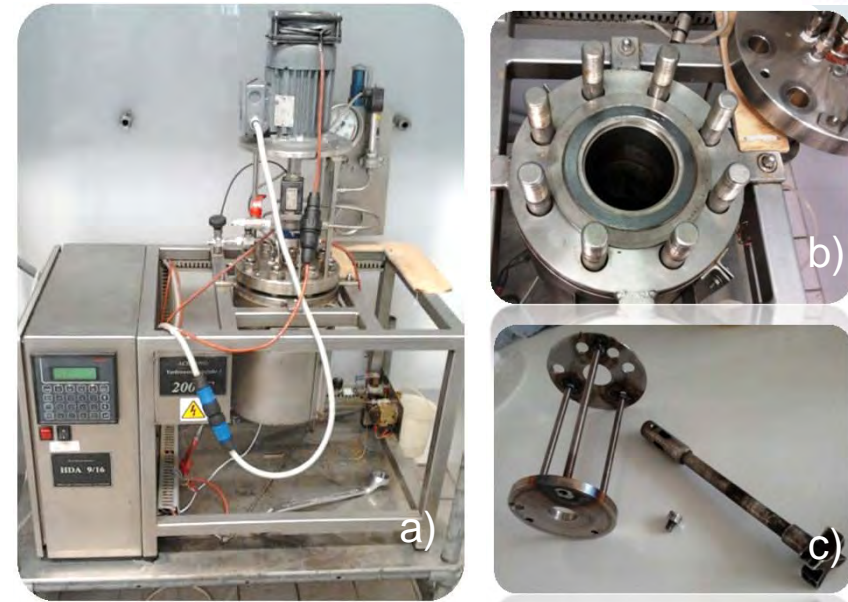
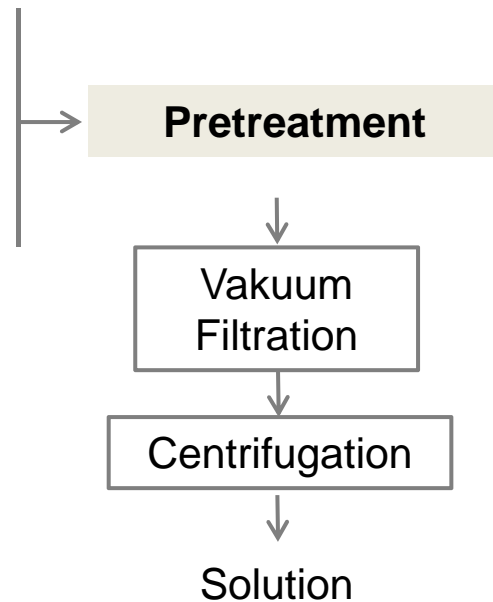


Fig. 6. High pressure autoclave (a) used, its reaction chamber (b) and stirrer (c) used in this study

**Product T : 160-200°C**  
**Shell T: 220°C**  
**Treatment t: 30 -90 min**  
**Ethanol/Water: 0-80/100-20**  
**Solid:Liquid: 1:10**  
**Particle Size: 3 mm**

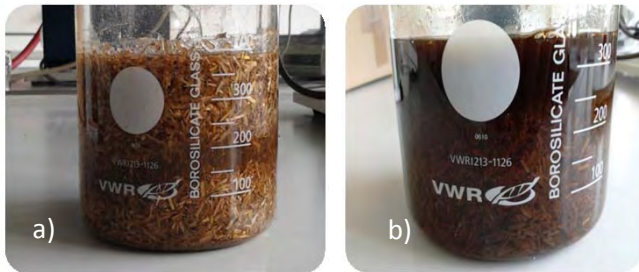
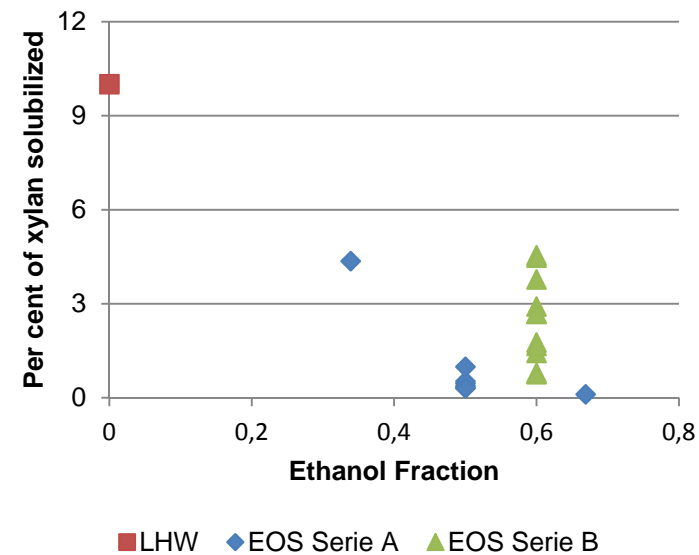
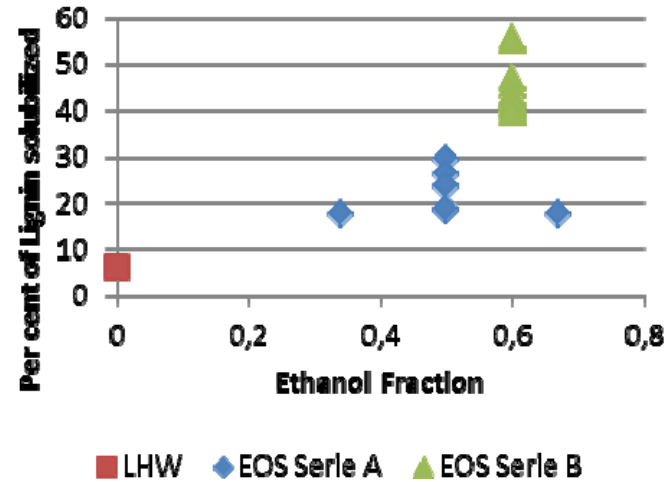
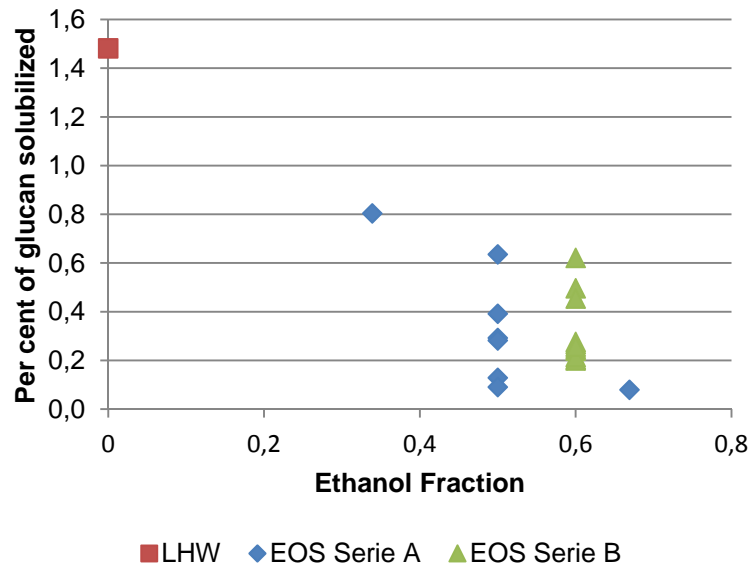
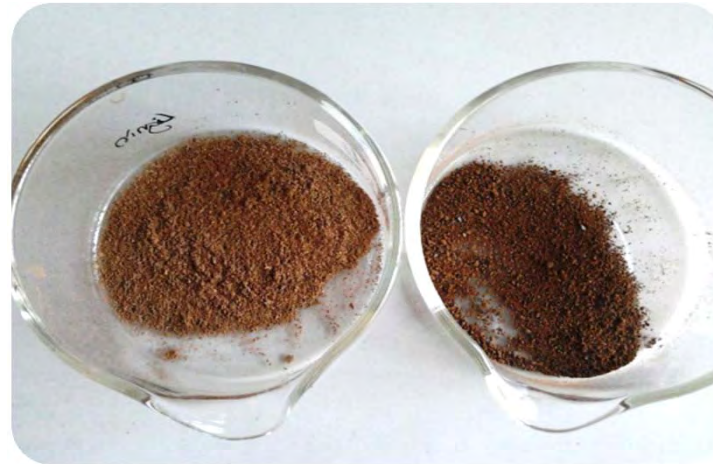


Fig. Mixture for (a) and nach Behandlung (b).



Ref.: Weinwurm, Silva, Cunha TU-Wien 2010-12





**Fig.** Lignin sample obtained pH 1 (right) and pH 2 (left).

<i>Lignin sample</i>	<i>Polysaccharides content [%]</i>			<b><i>Purity [%]*</i></b>
	<b>Uronic acids</b>	<b>sugars</b>	<b>Total</b>	
pH 1 precipitate	0.6	2.1	2.8	<b>97,2</b>
pH 2 precipitate	0.8	4.5	5.3	<b>94,7</b>

\* in terms of carbohydrates presence.

Ref.: Silva, Weinwurm, TU-Wien 2012

## Goals

- Concentration of the solution prior to precipitation
- Solvent stable membranes
- Membrane processes
  - Ultrafiltration
  - Nanofiltration
  - Reverse Osmoses



## Membrane separation

- Ultrafiltration
- Nanofiltration



A - Retentat (left) and  
Permeat (right)



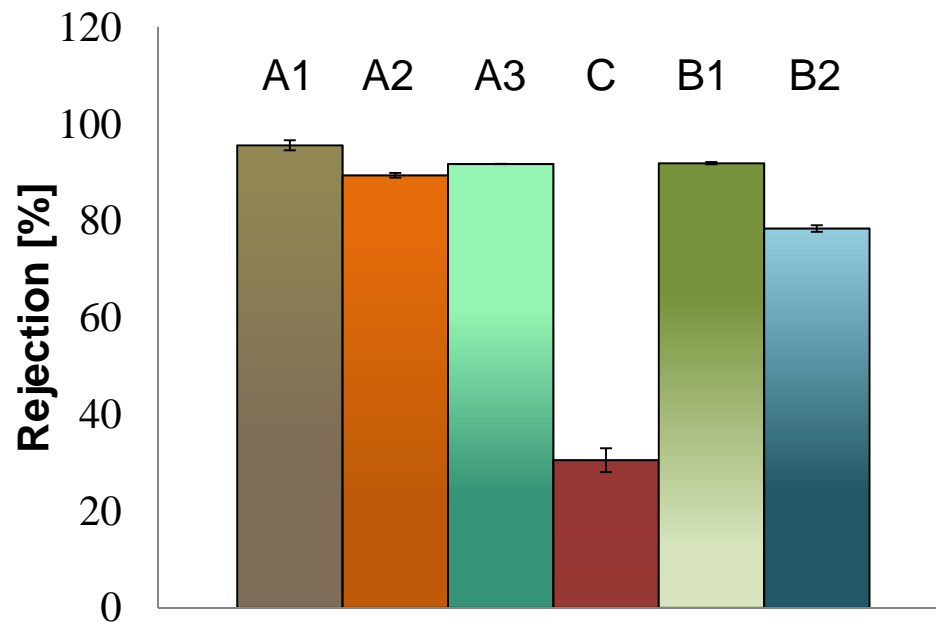
B - Permeat (left)  
and Retentat (right)



C - Permeat (left) and  
Retentat (right)

Ref.: Silva, Weinwurm, TU-Wien 2012

## Rejection Coefficient



Ref.: Silva, Weinwurm, TU-Wien 2012

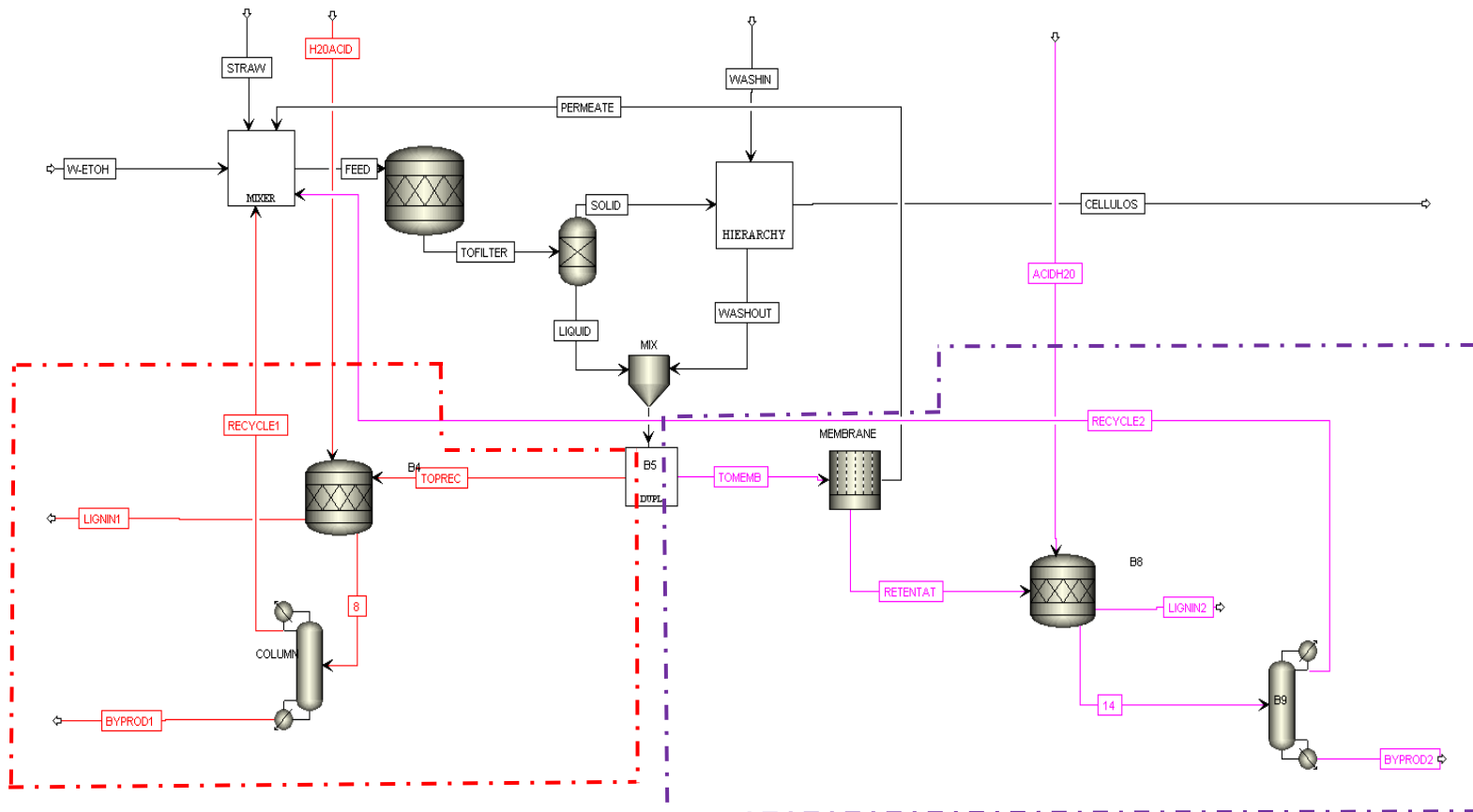


Example  
before end after filtration



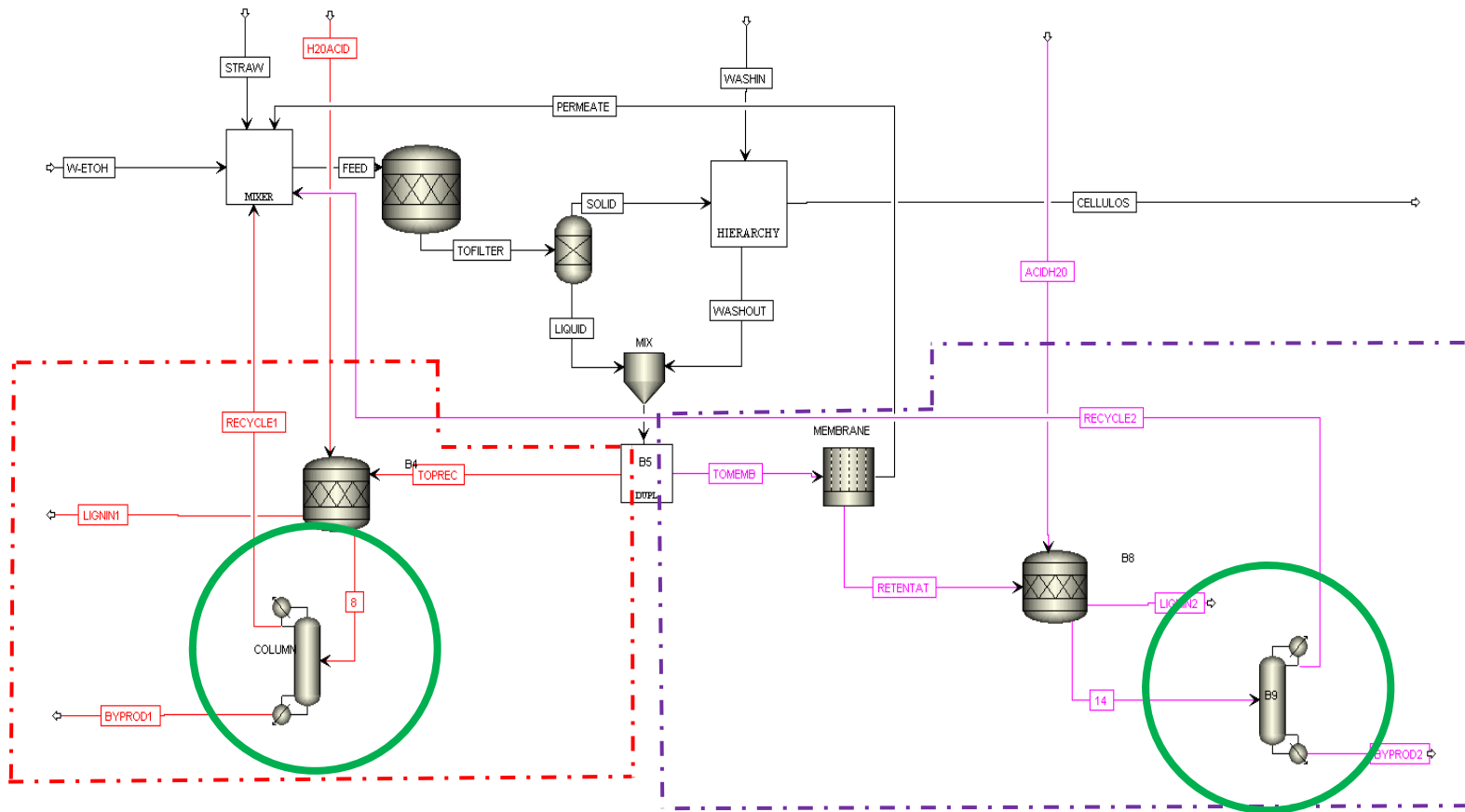
Example  
before end after filtration

# Process Optimization by Process Simulation



- - - Option I, classical route
- - - Option II, membrane process route

Ref.: Drljio, Wukovits TU-Wien 2012

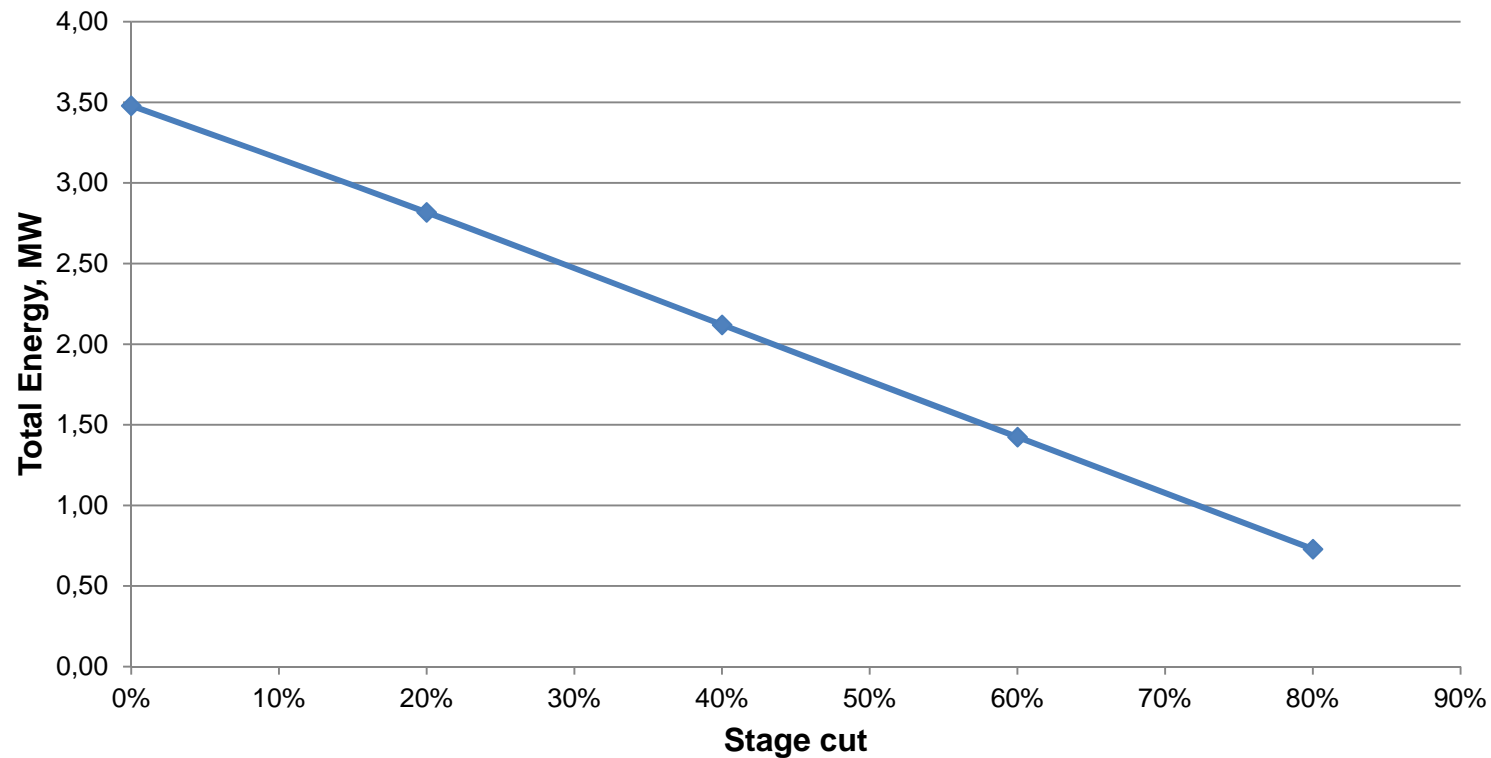


- - - Option I, classical route
- - - Option II, membrane process route

Ref.: Drljio, Wukovits TU-Wien 2012

## Membrane separation

Stage Cut: Permeate flow / Feed flow



Ref.: Drljo, Wukovits TU-Wien 2012



- Separation processes and closing cycles of treatment liquors are essential for the development of economical biorefineries.
- Processes simulation can support the optimization of biorefineries.
- For commercial products the product concentration and quality is very important – need for efficient separation and concentration processes (Research tasks)
- Improvement of process efficiency leads to closed process stream cycles and recovery of chemicals as well as process energy (Process development tasks)