

Biomethane for CNG and Grid Injection using Membrane Processes: New Developments and Technology Rollout

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Agenda

- Short intro why biogas upgrading?
- Quality issues
- Gas permeation process
- Scale-up to pilot and full scale process integration
 - Two-stage grid injection (Bruck/Leitha)
 - Single-stage CNG production (Margarethen/Moos)
- Energy demand
- Biogas pretreatment (desulphurisation)
- Costs
- Technology roll-out & future

Why biogas upgrading?

- Standardised product "biomethane" (compatible with natural gas)
- Higher efficiencies in energy utilisation than conventional gas engines without heat integration
- Access to new markets the gas grid
- Automotive utilisation (CNG)



Biogas Composition and Gas Grid Standards

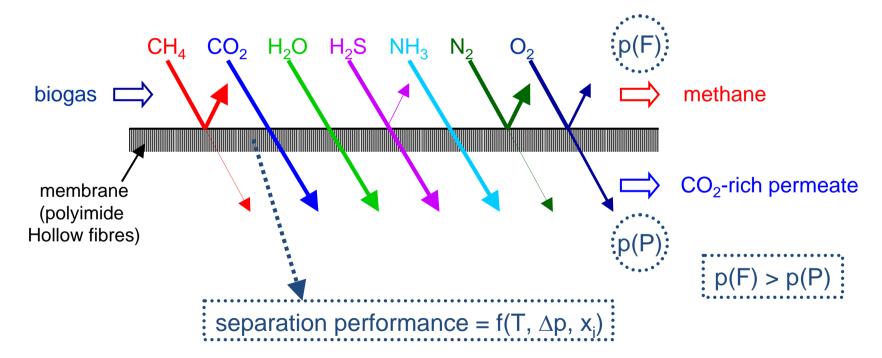
Parameter	Biogas	Quality according to Austrian Standard ÖVGW G31. / G33	Unit
Methane (CH ₄)	50 - 65	>97	[%]
Carbon dioxide (CO ₂)	25 - 45	≤ 2,0	[%]
Ammonia (NH₃)	< 1.000	technically free	[mg/m³]
Hydrogen sulphide (H ₂ S)	< 2.000	≤ 5	[mg/m³]
Oxygen (O ₂)	< 2	≤ 0,5	[%]
Nitrogen (N_2)	.	≤5	[%]
Water (H ₂ O) - Dewpoint	< 37 @ 1 bar	≤ - 8 bei 40 bar	[°C]
Upper Heatinhg value	6,7 - 8,4	10,7 - 12,8	kWh/m³
Wobbe-Index	6,9 - 9,5	13,3 - 15,7	kWh/m³

ÖVGW G31 defines natural gas, ÖVGW G33 specifies grid injection standards for biogases



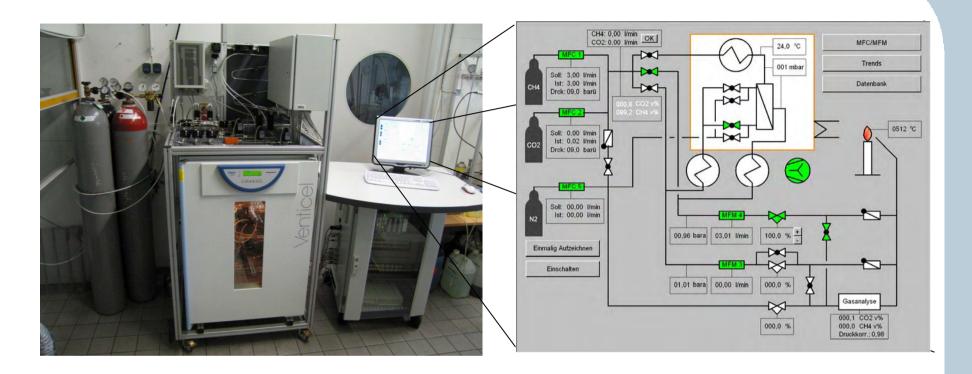
Upgrading of Biogas using Gas Permeation (GP)

- Separation principle: different permeabilities of methane and components to be separated.
- Important parameter: permeability ratio = selectivity.
- After compression biogas is fed to membrane modules.





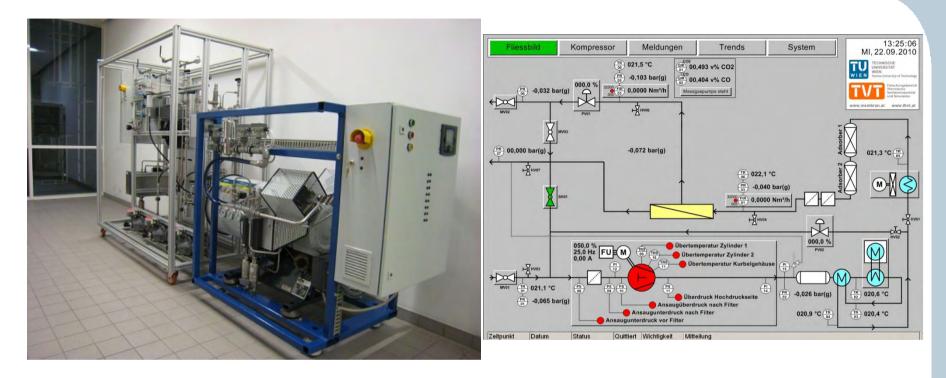
Membrane Test Equipment at TU Wien



- Preparation of CO₂/CH₄/N₂ gas mixtures with mass flow controllers
- Thermostatic chamber
- Industrial NDIR gas analyzer for CO₂ and CH₄
- Test control, visualization and data collection using a PLC with HMI/SCADA system



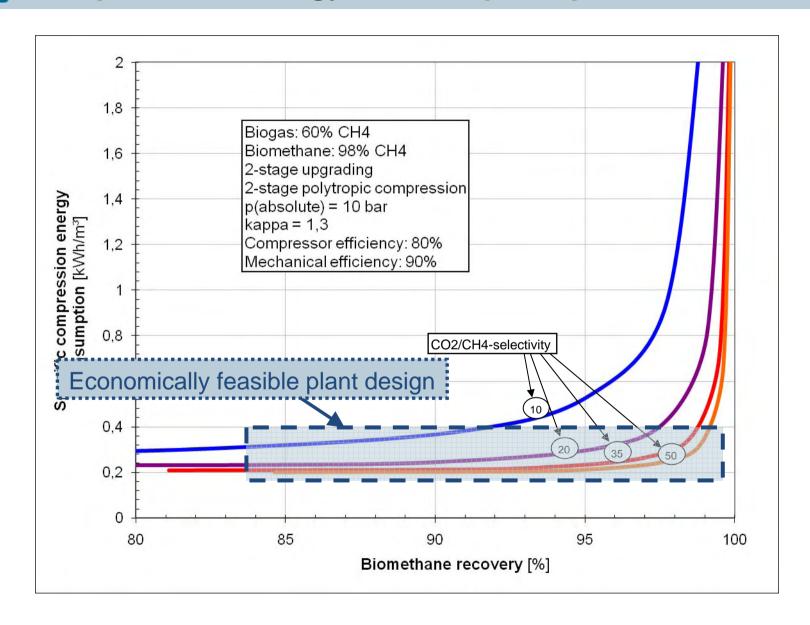
Pilot Test Equipment at TU Wien



- Mobile pilot plant for flexible treatment of many gas mixtures including H₂
- Magnet-coupled two-stage piston compressor (up to 15 bar, 0-6 m³/h)
- Fully automated upgrading plant for remote operation (industrial PLC)
 - 3 adsorber fillings in series
 - Cryo condenser
 - Reheater
 - One/two stage membrane separation with/without gas recycling
 - NDIR online continuous gas

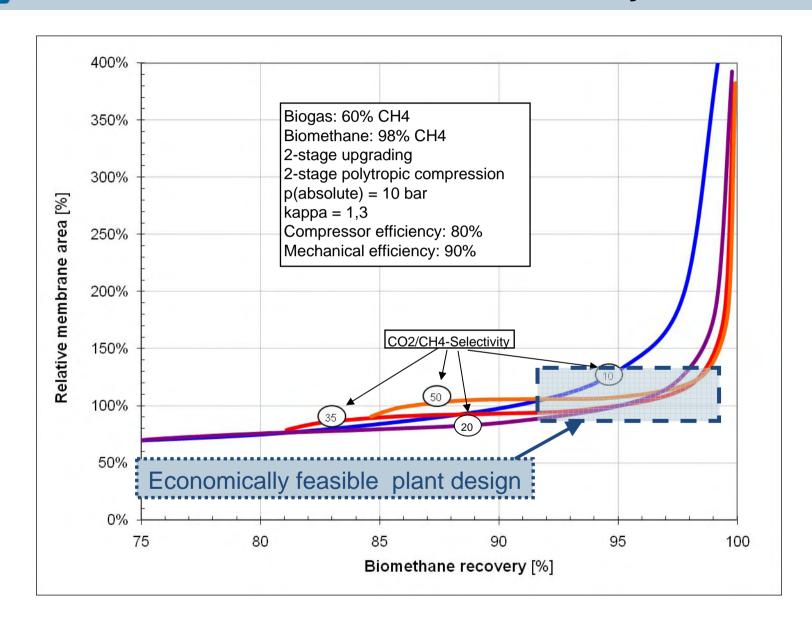


Compression Energy Consumption per m³ Product





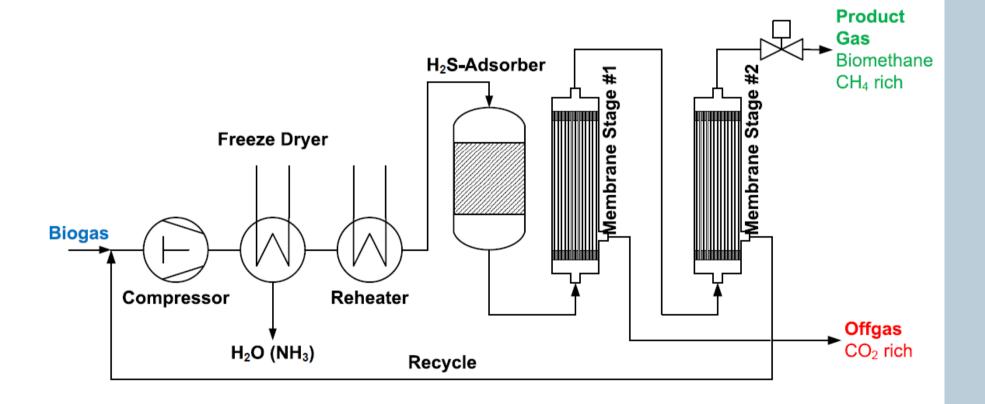
Membrane Area as Function of Recovery





Process Scheme of a Two-stage Membrane System

 Two-stage separation process with recycle and a single compressor





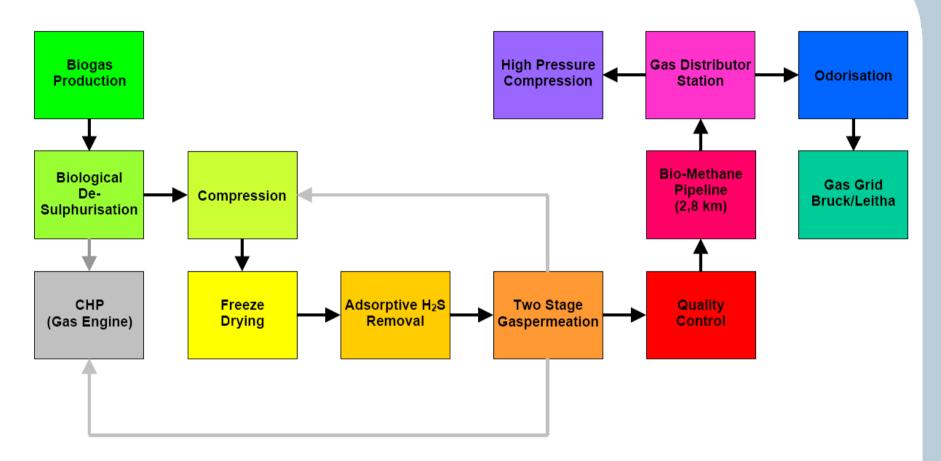
Biogas Upgrading Plant in Bruck/Leitha (Austria)







Process Integration (Two-stage design)



- Biological desulphurisation prior to membrane treatment
- Permeate is recycled to CHP plant "zero methane" emission of upgrading system

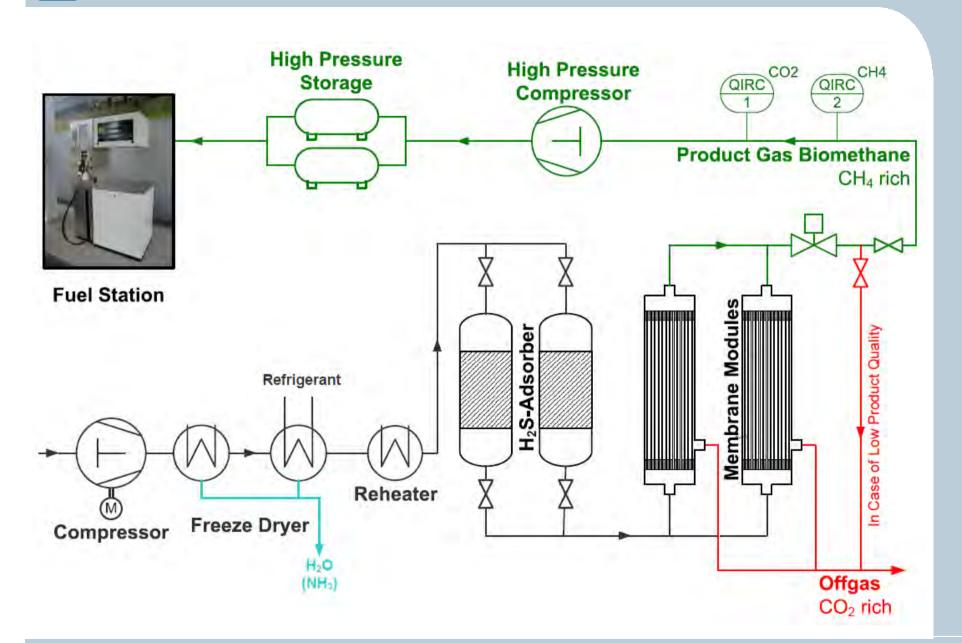
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Energy Consumption Analysis

- Main energy consumer of upgrading is the raw biogas compressor.
- Energy demand for constant product gas quality and quantity depends also on raw biogas methane content.
- Effect of plant layout (number of stages) on energy consumption:
 - Two stage gas grid injection plant: 0,378 kWh/m³STP of product gas
 - Single stage Bio-CNG-plant: 0,280 kWh/m³STP of product gas
- Energy consumption of <0,2 kWh/m³ STP of raw biogas possible!
- Related to the methane content of the produced biomethane gas stream:
 - Two stage gas grid injection plant: 3,2% (98,1vol% CH4)
 - Single stage Bio-CNG-plant: 2,8% (96,1vol% CH4)
- All values are valid for a product gas delivery pressure of about 3 bar(g).



Biomethane Fuel Station: Single Stage Upgrading





Biomethane Fuel Station using Membrane Technology

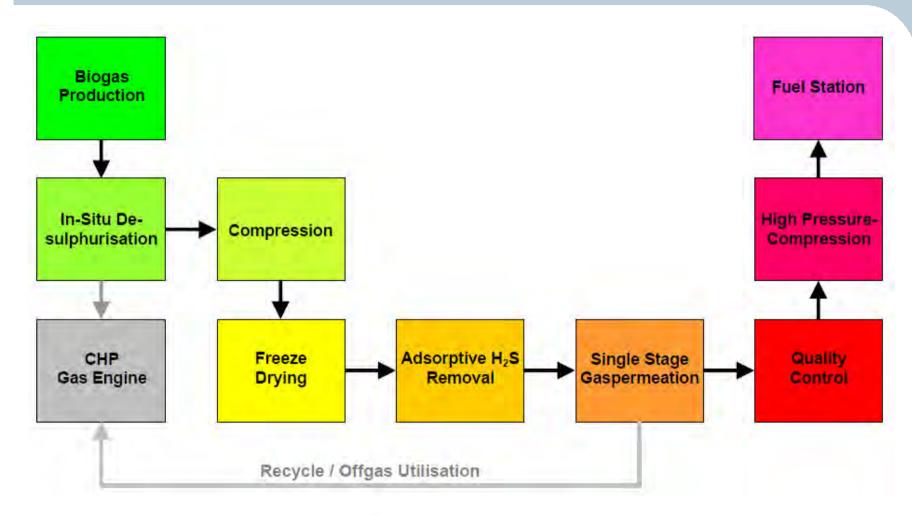


Permeate recycle to CHP plant

Further information: www.methapur.com
 Biomethane fuel station Margarethen/Moos



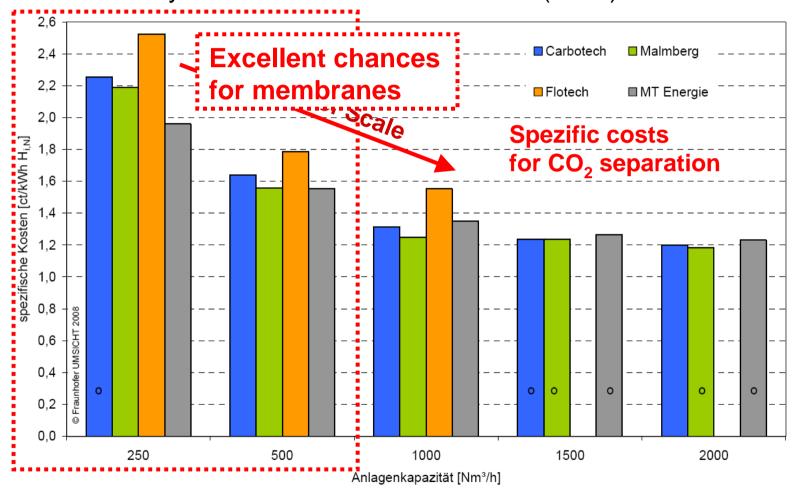
Process Integration (Margarethen am Moos)



- In-situ desulphurisation (addition of iron salts into the fermentation broth to catch suphides)
- Permeate is recycled to CHP plant "zero methane" emission of upgrading system

Costs for CO₂ Separation

Calculations by Fraunhofer Institut UMSICHT (2008)



Offgas Treatment & Costs

- Offgas treatment depends on process integration:
 - Mixing with biogas and utilisation in CHP plants
 - Thermal oxidation (flameless oxidation systems or direct combustion of low-cal gas)
 - Catalytic oxidation
 - Further treatment using additional membrane separation stage
- Specific costs of upgrading (depends on plant capacity):
 - Investment (depreciation 10 years, 8%):
 - 0,05 0,08 **€**m³ biomethane
 - **Operation** (> 8000 h/a):
 - 0,10 0,14 **€**m³ biomethane



Compatible Desulphurisation Technologies

Compatible:

- External biological desulphurisation in combination with pure oxygen injection
- In-situ desulphurisation using iron salts
- External chemical scrubber with oxidation using NaOH/H₂O₂, recommended for fluctuating H₂S concentrations in the biogas
- Adsorptive desulphurisation technologies with low excess of O₂ (impregnated activated carbon adsorbents)

Not suitable / incompatible:

- Air injection
- External biological desulphurisation with air injection







Reference Plants

In operation:

- since 2004: Pilot plants (up to 6 m³/h biogas, Vienna University of Technology)
- 2007: Bruck an der Leitha (180 m³/h biogas, 100 m³/h biomethane)
- 2007: Margarethen am Moos (80 m³/h biogas, 35 m³/h bio-CNG)
- Start-up 05/2010: Kißlegg / Baden-Württemberg, Germany (500 m³/h biogas)

Start-up:

Feed-in operation starts in 03/2011:
 Wiener Neustadt (220 m³/h biogas)

Supplier:

Axiom Angewandte Prozesstechnik GmbH







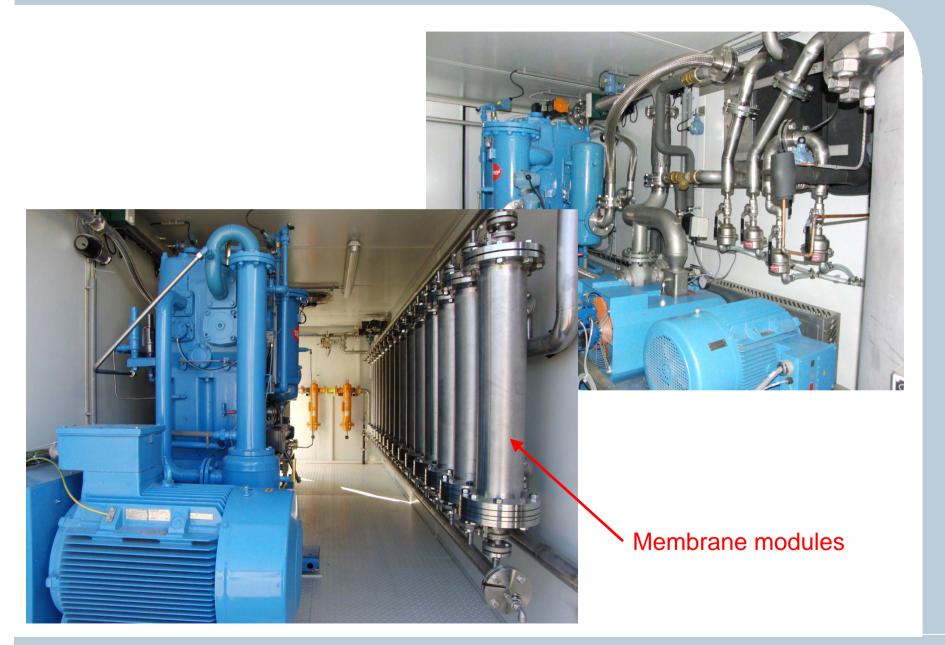


Capacity 500 m³/h biogas, 300 m³/h biomethane, approx. 8 km
 pipeline for grid injection and high pressure compression to 60 bar

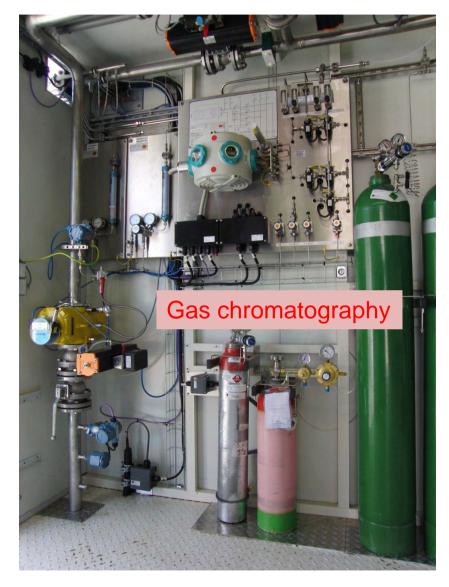














Further Information...

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Technology (turn key plants):
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Construction site of upgrading plant in Wiener Neustadt (Lower Austria)

Thank you for your attention!