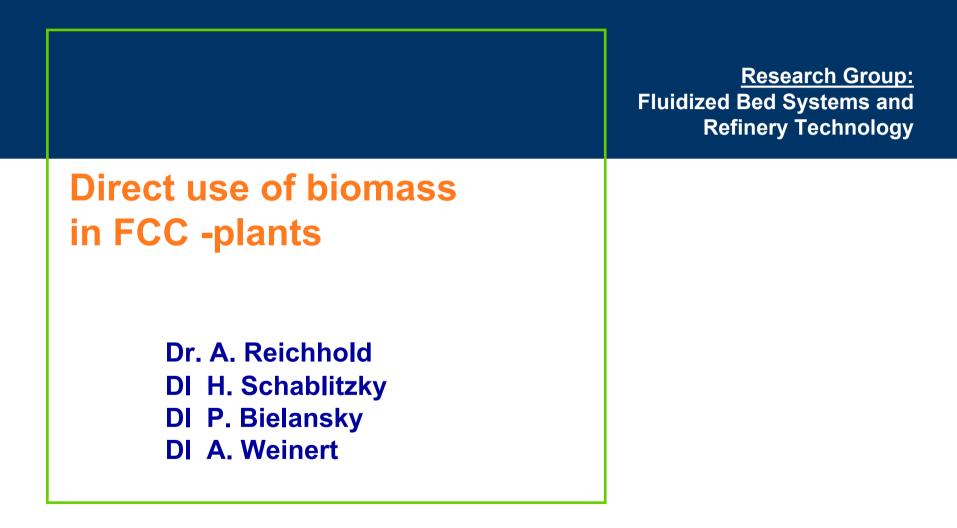
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Content

Catalytical Cracking of Bio Oils

- Based on Biomass: Natural Oils (Rape Seed Oil, Sunflower Oil, Soya Oil, Palm Oil), Fatty Acids, Used Frying Oils, Animal Fat
- Results from Testruns with an FCC- pilot plant
- Addition of Bio Oils to Vacuum Gas Oil

up to 100 m%:

- Continuous Cracking of Bio Oils possible?
- Effects on Products?
- C Effects on the FCC Pilot Plant?



Content

Catalytic Cracking of Bio Oils to Fuels and Monomers for Polymer Industry

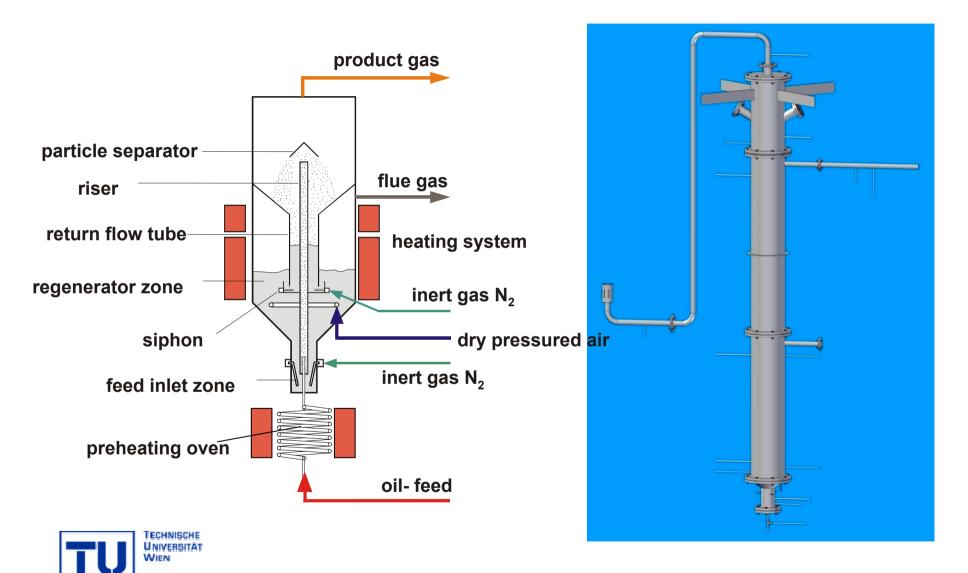
- Possibilities of an oil refinery:
 - Hydrogenation to split the ester bond
 - FCC to crack the big molecules of fatty oils
- After the treatment in the refinery the products appear to be similar to crude oil products
 - ► No difference in material compatibility
 - No biodegradability
 - Additives work as usual



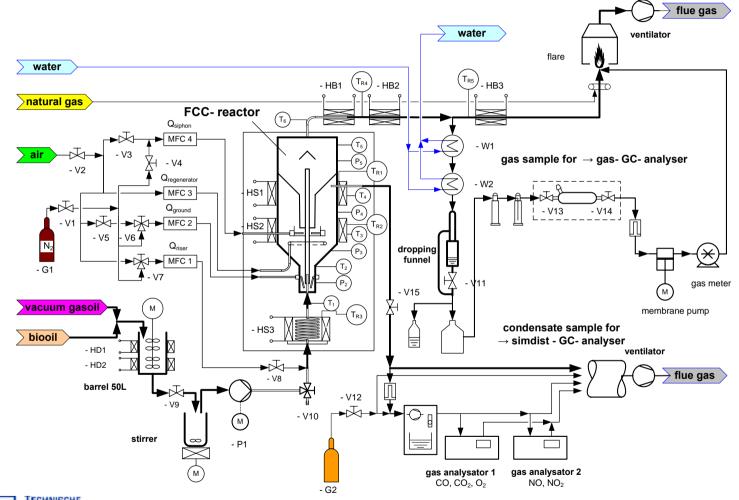
The Fluidized Bed System

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Experimental Setup



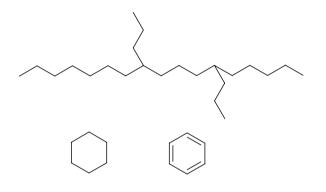


Chemical Composition of applied Oils

> Hydr. Vacuumgas Oil:

(Crude Oil- Product)

Density (20°C)	0.895 g/cm ³
Viscosity (100°C)	6.476 mm²/s
Aromatic Carbons	23.3 w%
Paraffinic and Naphtenic Carbons	>70 w%
Boiling Range	281°C-588°C

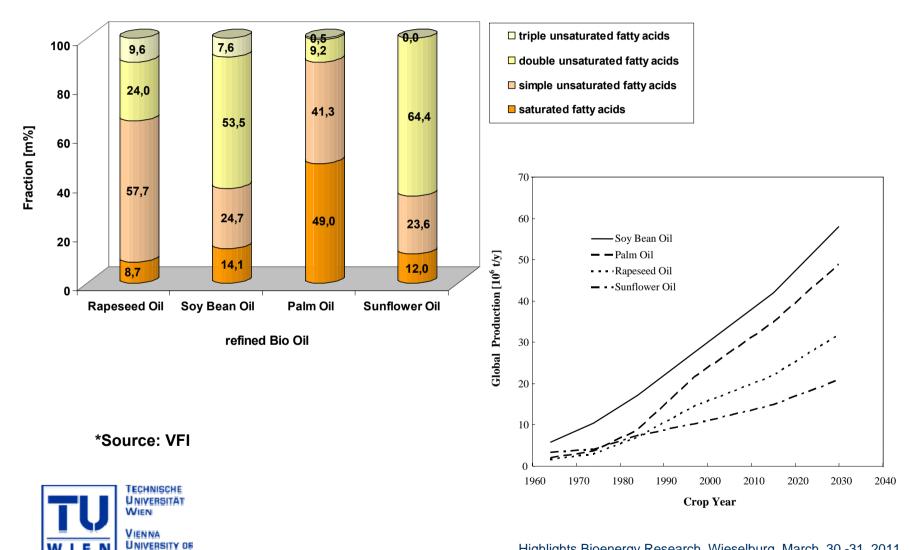


Bio Oil: fatty acid റ H₂Ç-O. Chain lenght of fatty acids stearic acid C12 – C22 0 **Boiling Point** < 300°C HĊ-O oleic acid 0 H₂Ċ-O linoleic acid glyceride TECHNISCHE



Bio Oil Composition (C12 – C22)

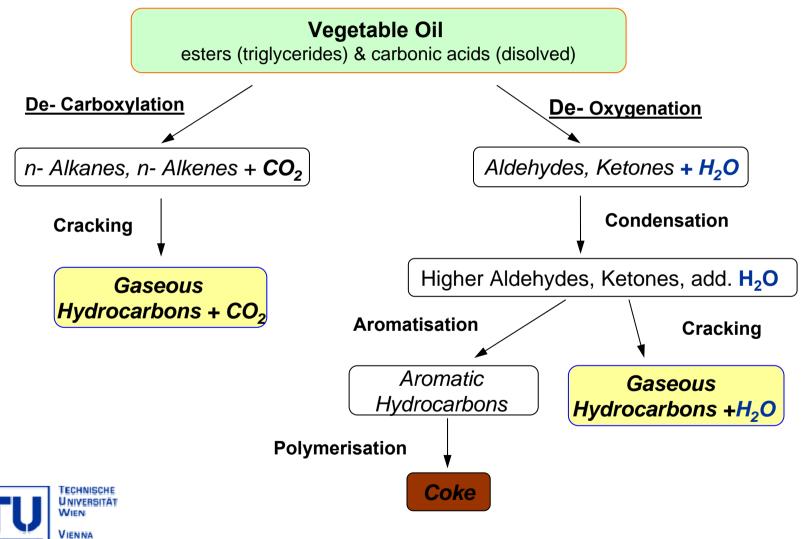
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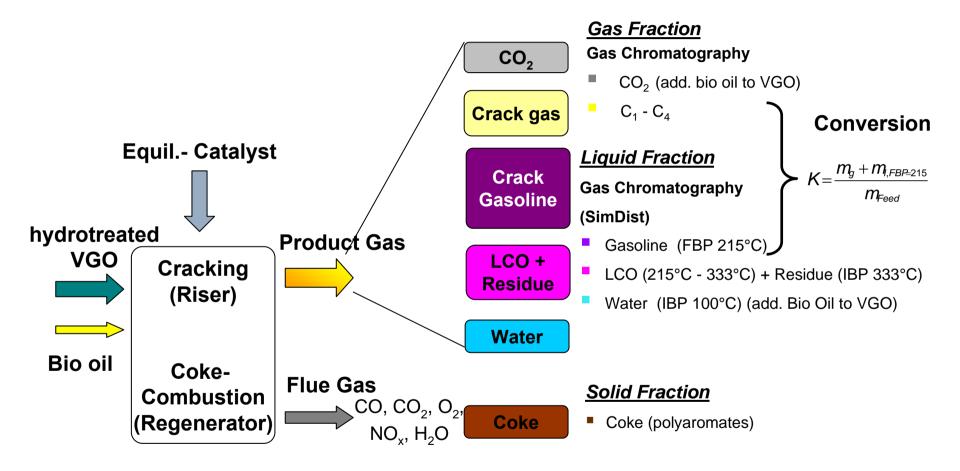
Suggested Reaction Pathes

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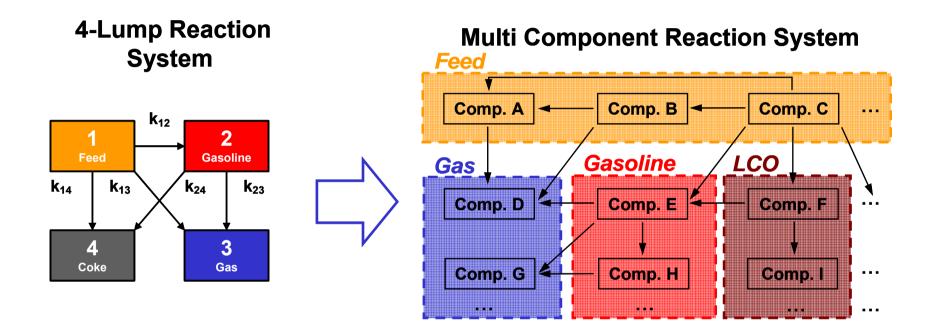


Cracking- Products (Lumps)



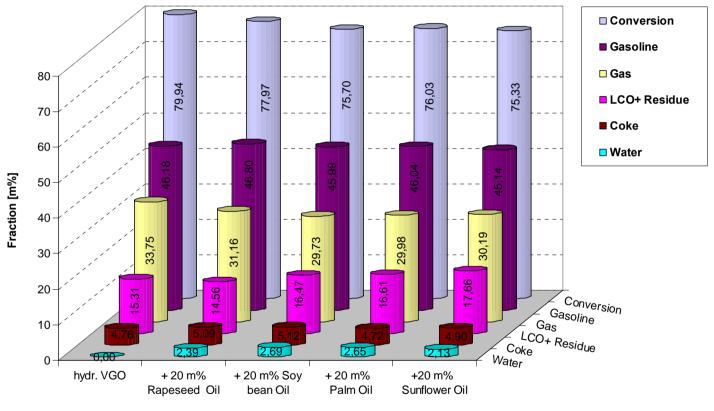


Cracking- Products (Lumps)



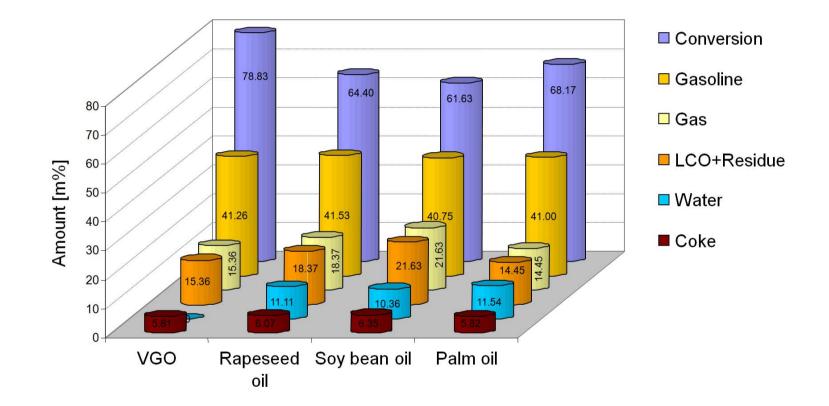
$$\frac{dy_{1}}{dt} = -k_{12,n} \cdot \Phi_{n} \cdot y_{1}^{2} - k_{13,n} \cdot \Phi_{n} \cdot y_{1}^{2} - k_{14,n} \cdot \Phi_{n} \cdot y_{1}^{2}$$



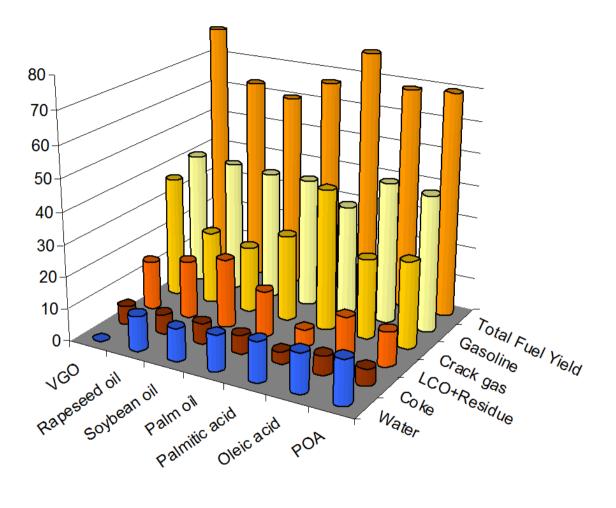


Feed

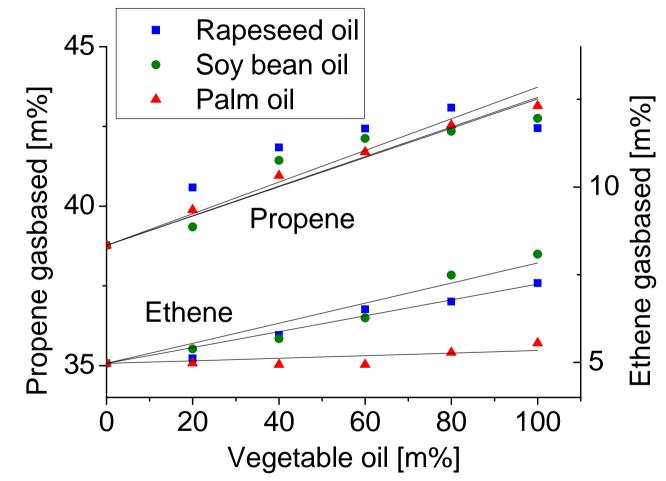






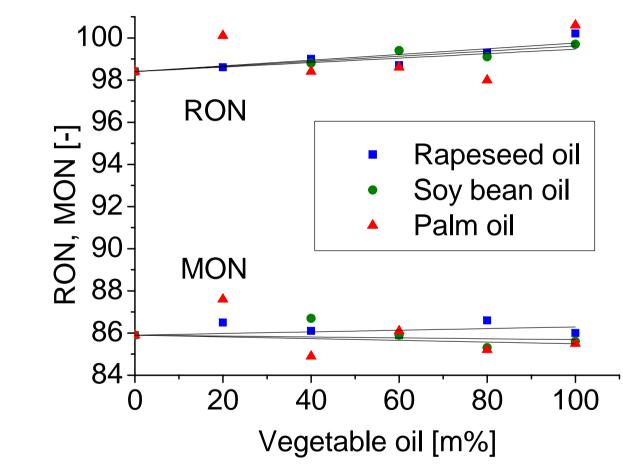






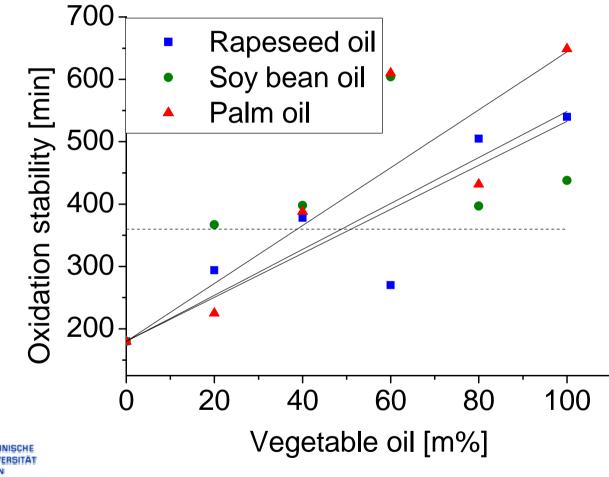


Product Quality





Product Quality





Conclusions

- The addition of bio oils has no significant influence on the routine operation of the FCC-plant
- It does result in a slightly modified product spectrum
- It has to be pointed out that the slight decrease in conversion was mainly caused by the oxygen content of the feed
- The production of up to 12 percent mass water from the oxygen in the bio oils does not constitute a problem in downstream processing of the products, since industrial FCC-units utilize steam for fluidization of the riser and the stripper
- The obtained liquid product contained a high octane (RON 99) gasoline fraction, which is comparable to high quality gasoline pools from traditional refineries
- The obtained light hydrocarbons contained a high percentage of propylene and ethylene - so the FCC process further offers a possibility to produce bio polymers without supporting the greenhouse effect.



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