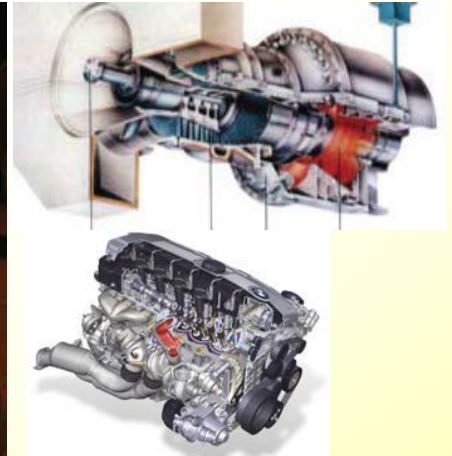


ERA-NET Bioenergy project “EnCat“

Enhanced catalytic fast pyrolysis of biomass for maximum production of high quality biofuels



Thomas Brunner

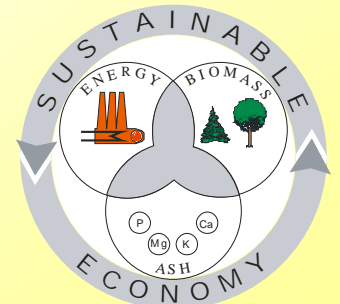
BIOS BIOENERGIESYSTEME GmbH

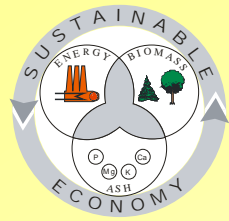
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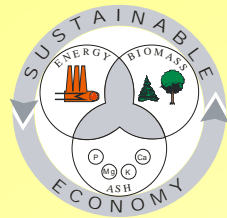




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Contents

- **EnCat key data and project consortium**
- **Background and intention**
- **Objectives**
- **Selected results achieved so far**
- **Outlook**



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EnCat key data and project consortium (I)

EnCat **Enhanced catalytic fast pyrolysis of biomass for maximum production of high quality biofuels**

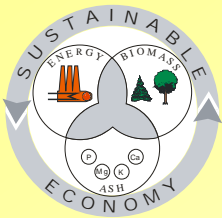
Duration: 42 months (project start: 02/2017)

The project is carried out in the core of the ERA-NET Bioenergy programme “10th Joint Call for Research and Development Proposals of ERA-NET Bioenergy”

Partner from Austria



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EnCat key data and project consortium (II)

Partners from the Netherlands



University of Twente (project coordinator)



Alucha Management B.V.



OPRA Turbines International BV

Partners from Sweden



KTH Kungliga Tekniska högskolan



RISE Research Institute of Sweden

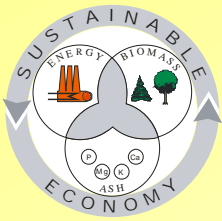
Partners from Poland



ICHPW Institute for Chemical Processing of Coal



HIG Polska Sp. z. o.o.



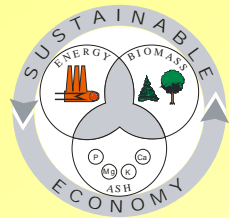
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Background and intention (I)

- **Fast pyrolysis of biomass** is one of the most promising ways to directly generate liquid fuels from biomass

- However, the produced **pyrolysis oil** may have **several drawbacks** which suppress its application for power and heat generation or transportation fuels
 - high oxygen content
 - high water content
 - high contents of water-soluble acids

- which affect negatively the**
 - acidity (corrosion effects)
 - miscibility with petroleum-based fuels (separation of fractions)
 - chemical stability (aging)
 - viscosity
 - energy density



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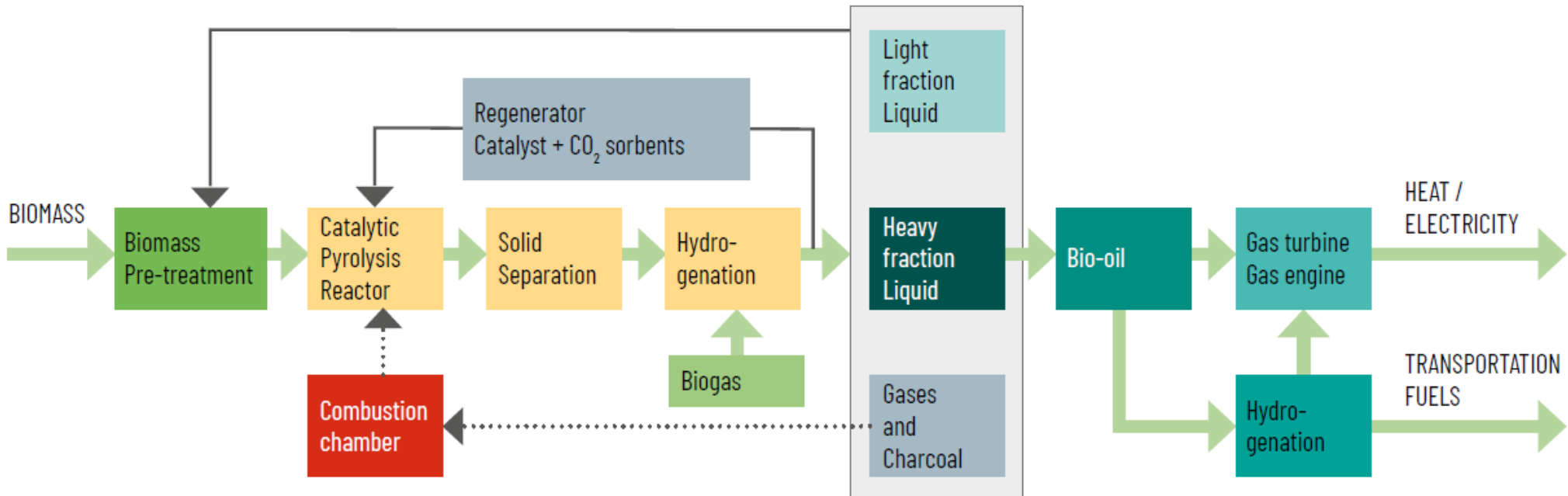
Background and intention (II)

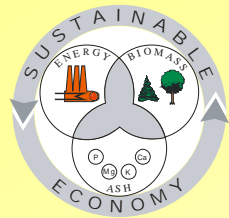
- The **Enhanced Catalytic Pyrolysis (EnCat)** project investigates a new concept for the production of high-quality bio-oil
- The **EnCat concept** consists of the following components
 - A novel **biomass pre-treatment** step to make the concept suitable for both woody biomass and biomass residues from agriculture
 - Biomass **pyrolysis** in a reactor making use of **deoxygenation catalysts**
 - Simultaneous **CO₂ capture with sorbents** and via the water-gas-shift reaction **in-situ production of hydrogen**
 - After cleaning, the oil vapours will be **mildly hydrogenated** to produce a high-quality bio-oil.
 - Utilisation of the bio-oil in **gas engines** and a **gas turbines**
 - Further upgrading by a new method of **downstream hydrogenation**



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EnCat concept

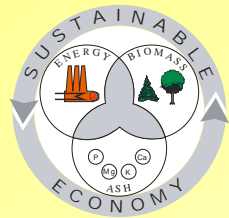




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Overall objectives

- Development of a new concept for the production of biofuels based on an enhanced catalytic flash pyrolysis process including deoxygenation and hydrogenation for the high-yield production of high-quality bio-oil from both woody and residual biomass streams
- To test the high-quality oil in gas turbines and diesel engines for the production of heat and power
- To further increase the applicability of the bio-oil as transportation fuel by downstream hydrogenation
- To evaluate the new concept from biomass to biofuels with respect to sustainability and techno-economic feasibility



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Scientific objectives (I)

- Get insight in the **catalytic pyrolysis** mechanisms of different biomass streams (woody biomass, agricultural residues)
➔ *University Twente, KTH*
- To develop a **leaching process** for the biomass feedstock in order to remove alkaline and alkaline earth metals (AAEMs) and to optimize this process
➔ *BIOS*
- Understand and develop the application of **CO₂ sorbents** in catalytic pyrolysis reactors for in-situ production of hydrogen
➔ *University Twente*
- Development of a **downstream hydrogenation** process for the production of bio-oil with low oxygen contents that can be used as transportation fuel
➔ *ICHPW*



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Scientific objectives (II)

- Improve **atomization and combustion of bio-oil in gas turbines** and to optimize existing gas turbines for (catalytic) pyrolysis oil applications with low emissions and high efficiencies via experimental research and numerical (CFD) simulations
➔ *OPRA, BIOS, University Twente*
- To investigate bio-oil combustion in **gas engines**
➔ *ICHPW*
- To design a **full-scale plant** based on enhanced catalytic pyrolysis and to develop a roadmap for further commercialization
➔ *Alucha*
- Evaluation of the new concept from biomass to biofuels with respect to sustainability and techno-economic feasibility
➔ *RISE, BIOS*



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Selected results – Biomass pre-treatment – BIOS (I)

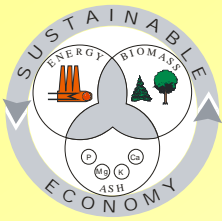
Objectives

- High contents of **alkaline and alkaline earth metals** (AAEM – Ca, Mg, K and Na) in agricultural biomass feedstocks cause problems during pyrolysis (reduced oil and sugar yield)
- Development and lab-scale test of **leaching** methods with the aim to **reduce the AAEM contents** of agricultural biomass feedstocks to make them applicable for the pyrolysis process

Methodology

- Leaching tests of woody and agricultural biomass with acids and water
- Comprehensive parametric study regarding the influence of
 - acidity
 - temperature and
 - residence time
 - fuel to leaching liquid ratioon the leaching efficiency



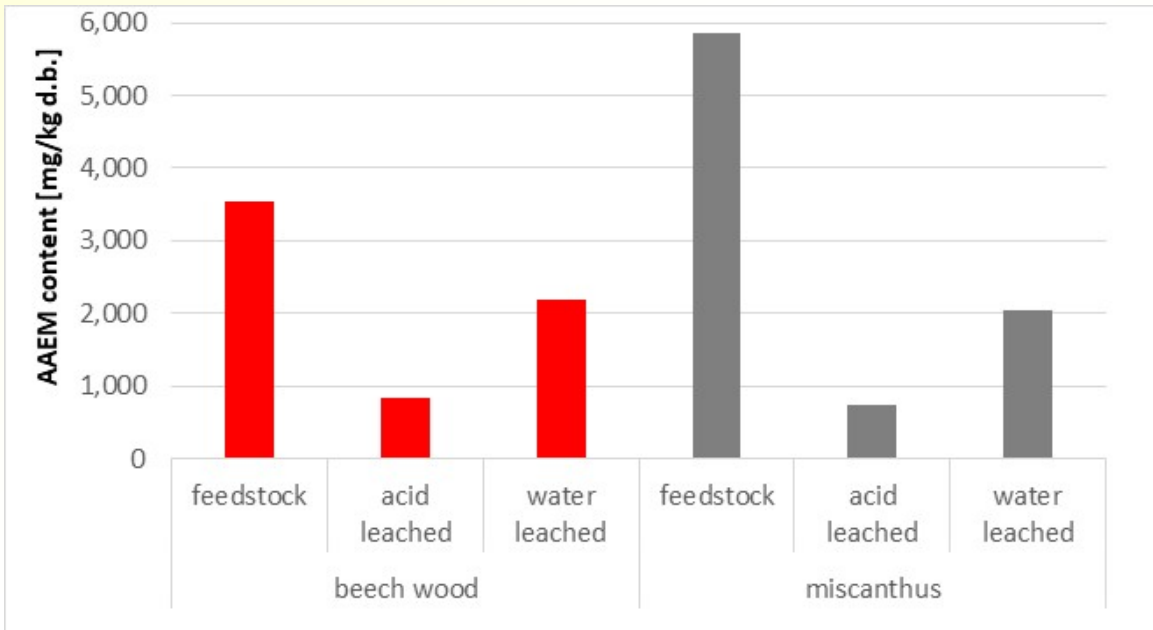


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Biomass pre-treatment – BIOS (II)

Preliminary results

- **Leaching of woody biomass (beech wood)**
 - with acids: 75% AAEM reduction
 - with water: 33% AAEM reduction
- **Leaching of agricultural biomass (miscanthus)**
 - with acids: 85% AAEM reduction
 - with water: 60% AAEM reduction



Leaching at mild conditions:
30°C, 30 minutes residence time,
acid leaching: 1% acetic acid in water

➔ **Even when leaching with water the AAEM contents of miscanthus can be reduced below the AAEM level of beech wood**

Objectives

- Experimental study of catalytic fast pyrolysis with MCM-41 and HZSM-5 zeolite catalysts
- Improve the bio-oil quality
- Determine the effects of catalysts on the bio-oil quality

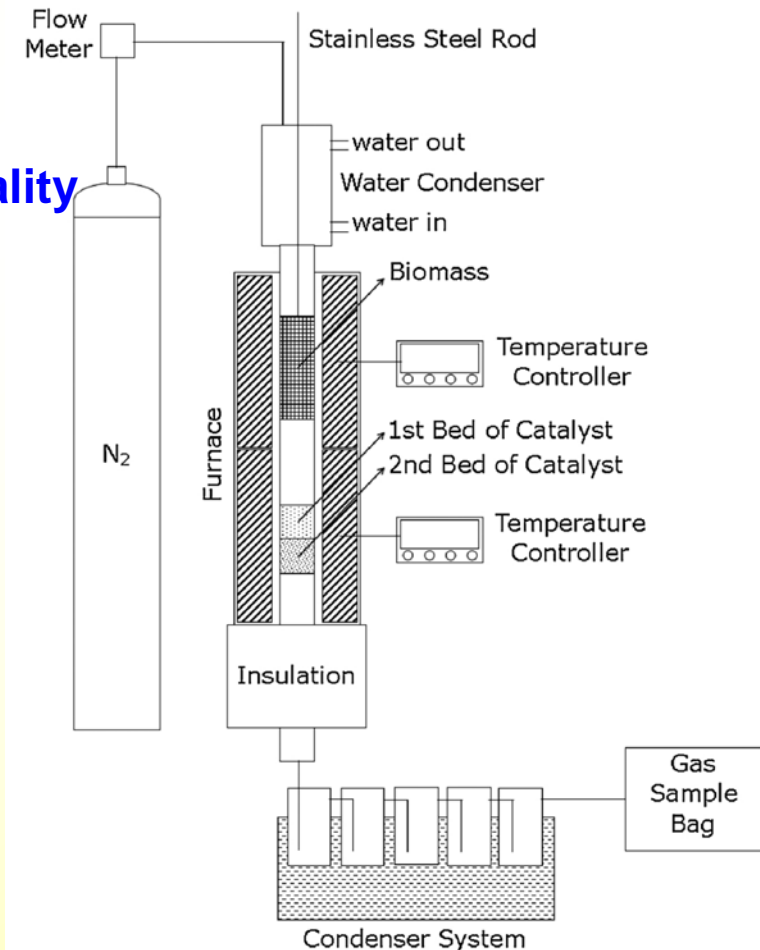
Methodology

Reactor heated up to the target temperature for the catalysts (500°C)

The evolved volatiles from the sample are passed directly to the ex-situ beds containing catalysts

The ratio of MCM-41 and HZSM-5 zeolite catalyst was altered to give the required ratio

The ratio of sample to catalysts was 1:1





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Enhanced catalytic pyrolysis – KTH (II)

Results for different catalyst ratios of H-ZSM-5 and Al-MCM-41

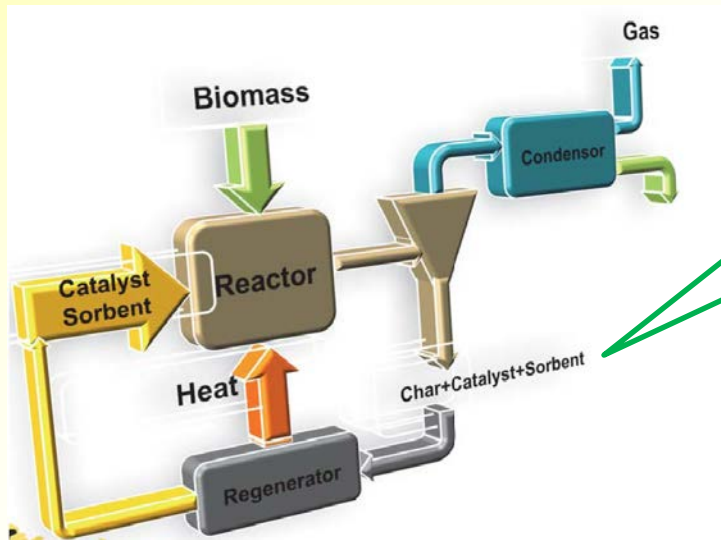
Experiment	Element (wt.%)				Deoxygenation degree (%)	HHV Dulong (MJ/kg)	Heavy Oil (g)	HHV Dulong (MJ)	Relative Energy
	C	H	O	N					
Non-catalytic	47,25	7,91	43,10	0,50	1,60	19,55	57,95	1,13	100%
H-ZSM-5	73,50	7,79	21,00	0,61	52,05	32,28	7,08	0,23	20%
HA 7:1	74,90	8,00	15,00	0,59	65,75	34,15	5,66	0,19	17%
HA 3:1	82,05	8,37	8,60	0,50	80,37	38,26	4,25	0,16	14%
HA 2:1	80,00	8,11	10,30	0,61	76,48	36,89	3,54	0,13	12%
HA 1:1	84,20	8,24	6,70	0,62	84,70	39,15	2,83	0,11	10%
Al-MCM-41	85,60	8,20	4,80	0,63	89,04	39,91	1,42	0,06	5%

Deoxygenation degree (%) = $(1 - (O\text{-biooil}/O\text{-biomass})) \times 100$

HHV Dulong = $338.2C + 1442.8(H - (O/8))/1000$

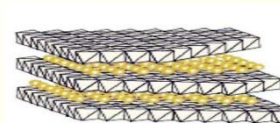
Aim of the work:

- Improve Quality of pyrolysis oil (reduce acidity i.e., carboxylic acids)



- **Catalyst:** Deoxygenation Reactions (e.g., remove acids)
- **Sorbent:** Capture CO_2 and shift equilibrium of WGS $\text{CO} + \text{H}_2\text{O} \rightleftharpoons \text{CO}_2 + \text{H}_2$ (Exothermic Reaction) for in-situ hydrogen (H_2) production

Hydrotalcite

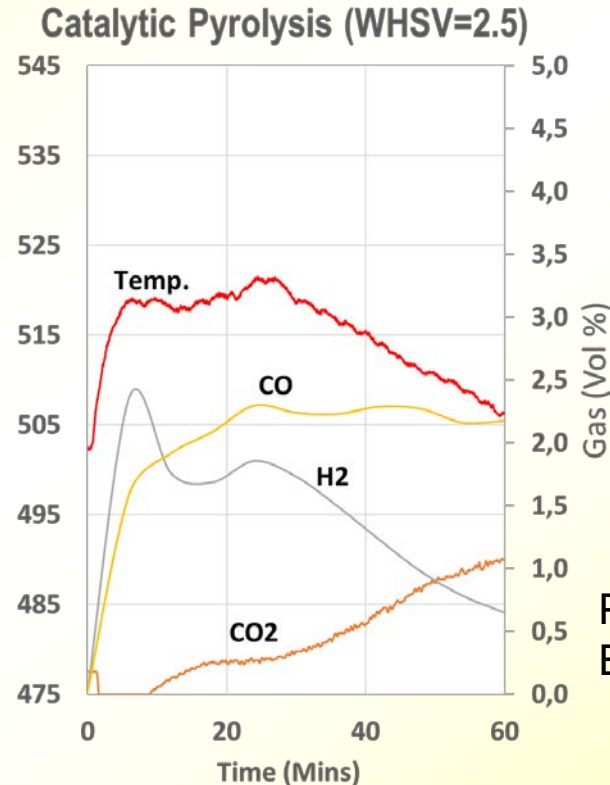
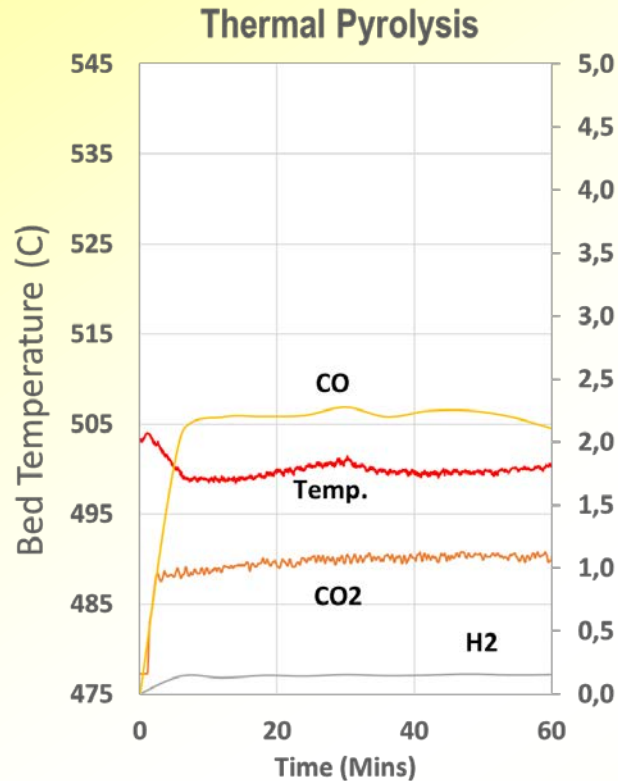


Dolomite



Hydrotalcite and Dolomite are selected due to their ability for both deoxygenation and CO_2 sorption reactions

Test results with Dolomite in a fluidized bed reactor

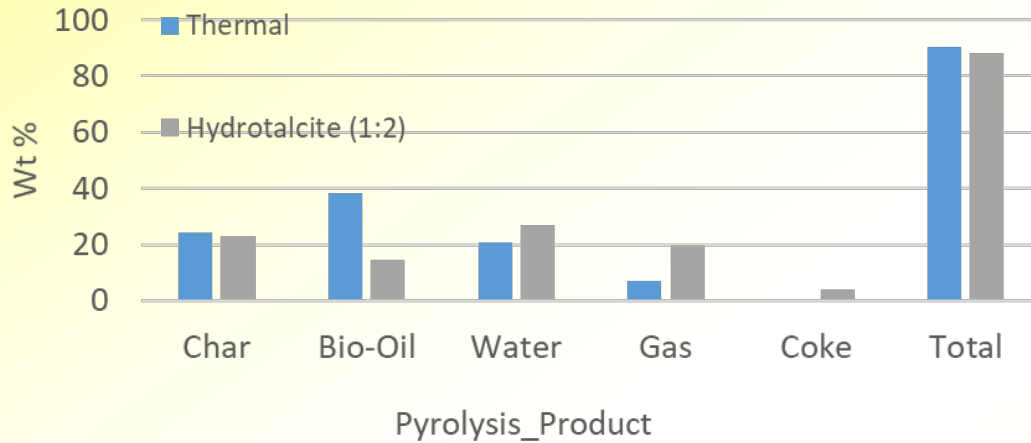


Pyrolysis Temperature: 500°C
Experimental Time: 60 Min.

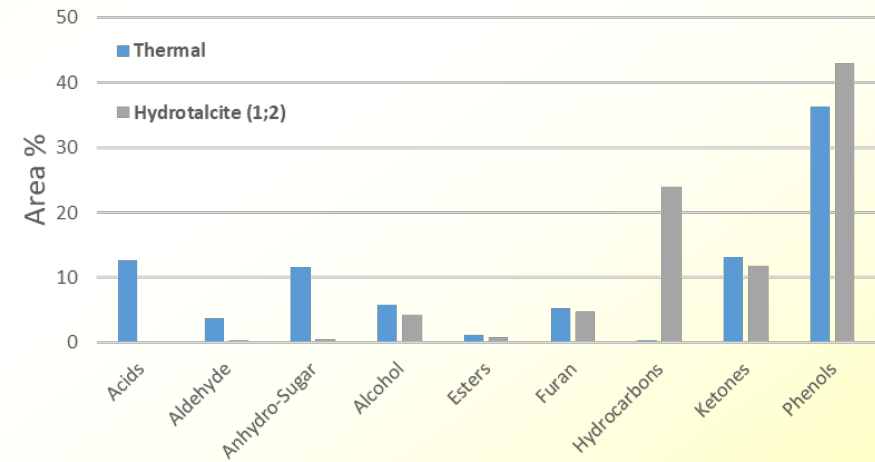
- Clear indication of equilibrium shift of WGS Reaction ($\text{CO} + \text{H}_2\text{O} \leftrightarrow \text{CO}_2 + \text{H}_2$)
- **40.4%** bio-oil yield
- **5.74 %** of H in the feed converted to Hydrogen via water gas shift reaction

Test results with Hydrotalcite

Mass Balance



Bio-Oil composition GC-MS (organic Phase)



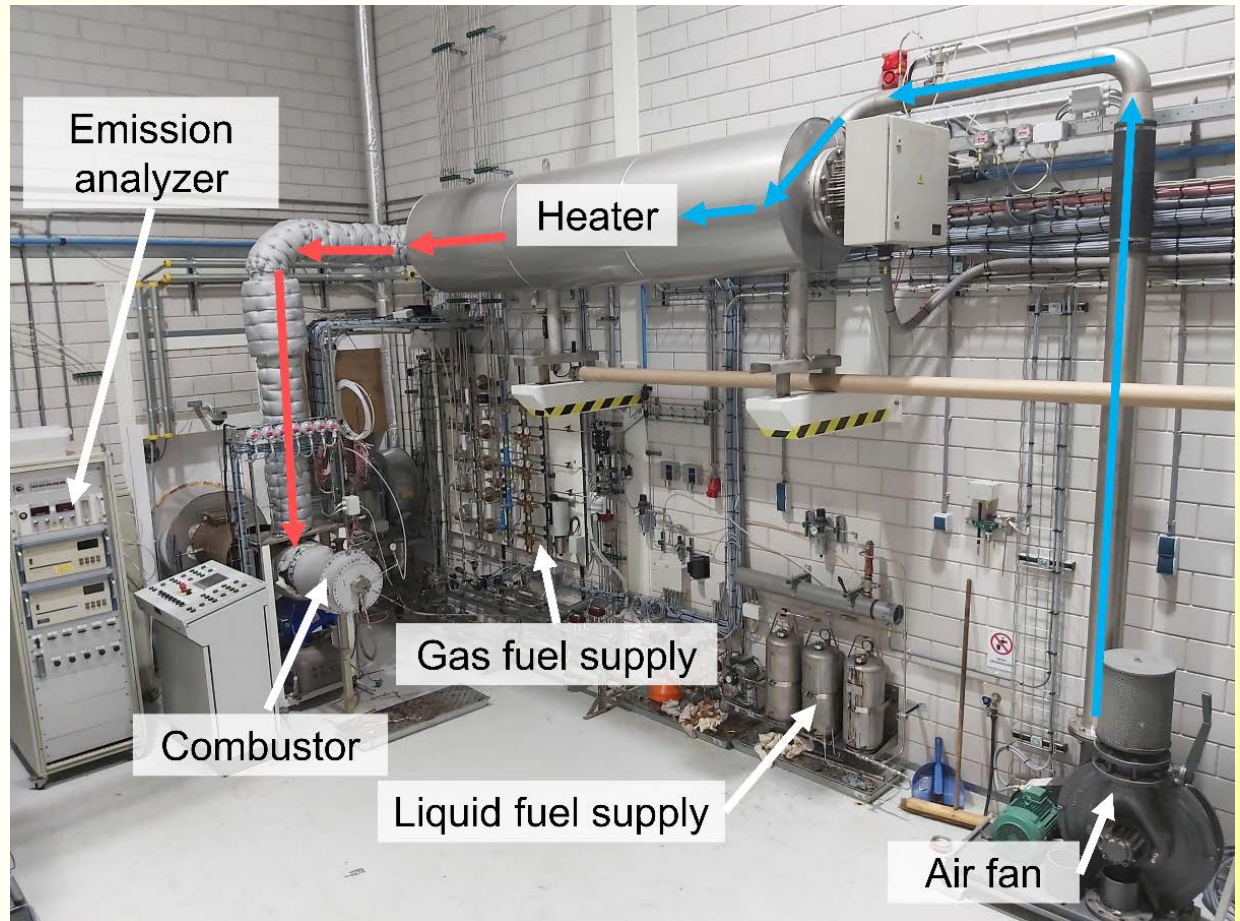
- **Minor increase in H₂ Production**
- **Increase in Hydrocarbon**
- **Elimination of Acids**



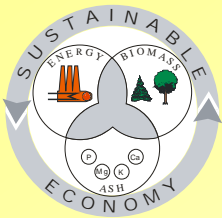
Full-scale gas turbine combustor tests at atmospheric conditions

Measurement of:

- Temperatures (inlet, outlet)
- Pressures
- Air and fuel mass flow
- Liner metal temperatures by thermochromic paint
- Emissions (CO, CO₂, NO, NO₂, O₂)



Atmospheric combustor test rig at OPRA



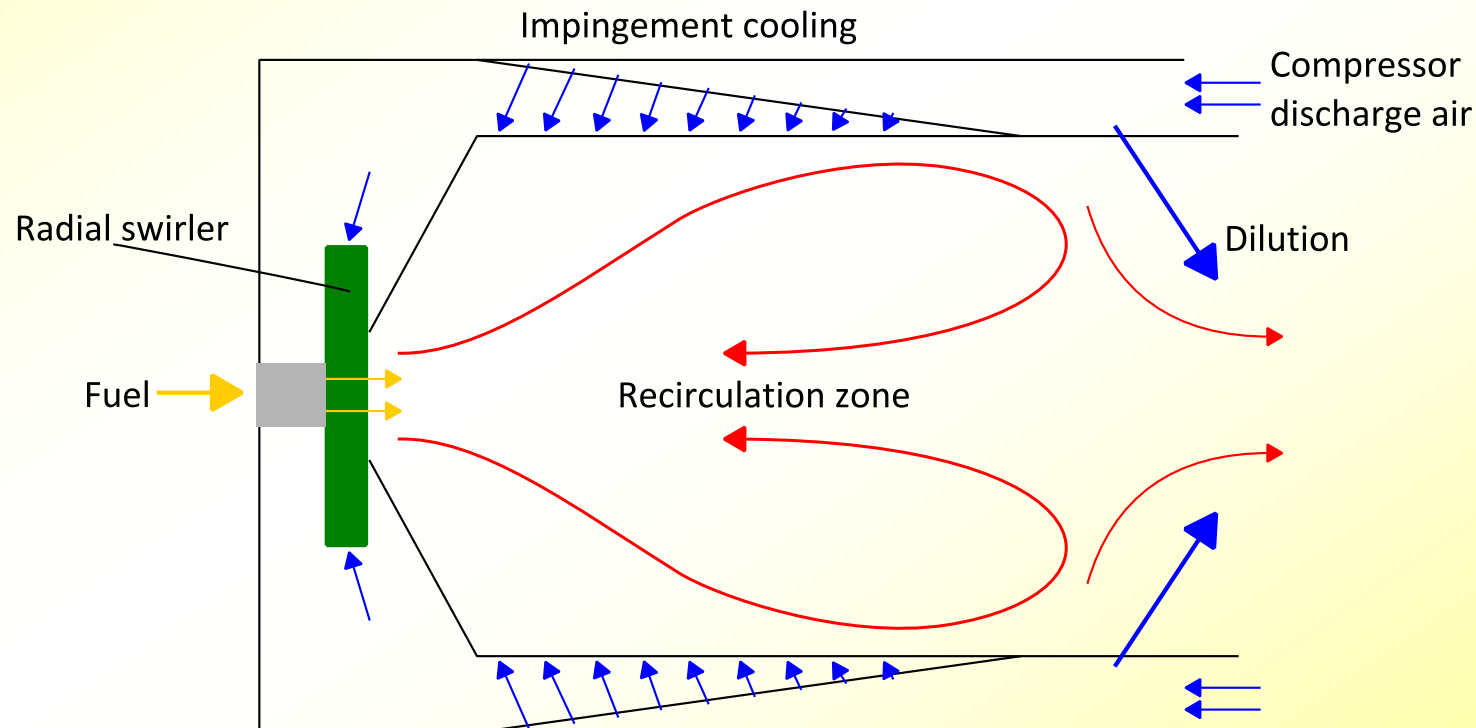
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Bio-oil combustion tests – OPRA (II)

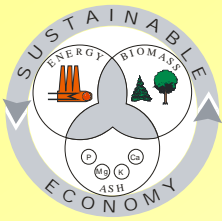
Design of the OPRA 3C low calorific fuel combustor

3C combustor* designed for burning low-calorific gaseous and liquid fuels

- Diffusion type combustor
- Significantly larger volume than conventional combustor
- Impingement cooling



*Patent US 8,844,260
Low calorific fuel combustor
for Gas Turbine



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Bio-oil combustion tests – OPRA (III)

Wood pyrolysis oil successfully tested during the EnCat project by applying a new nozzle design

- Good atomization is a key parameter for operating liquid fuels
- High viscosity and polymerization at high temperatures make pyrolysis oil atomization challenging
- New nozzle has been developed by OPRA which allows stable operation with 100% wood pyrolysis oil over wide load range
- Nozzle has been successfully tested in the atmospheric combustor test rig with multiple fuels
- CFD simulations of BIOS and UT for further combustor optimisation are ongoing



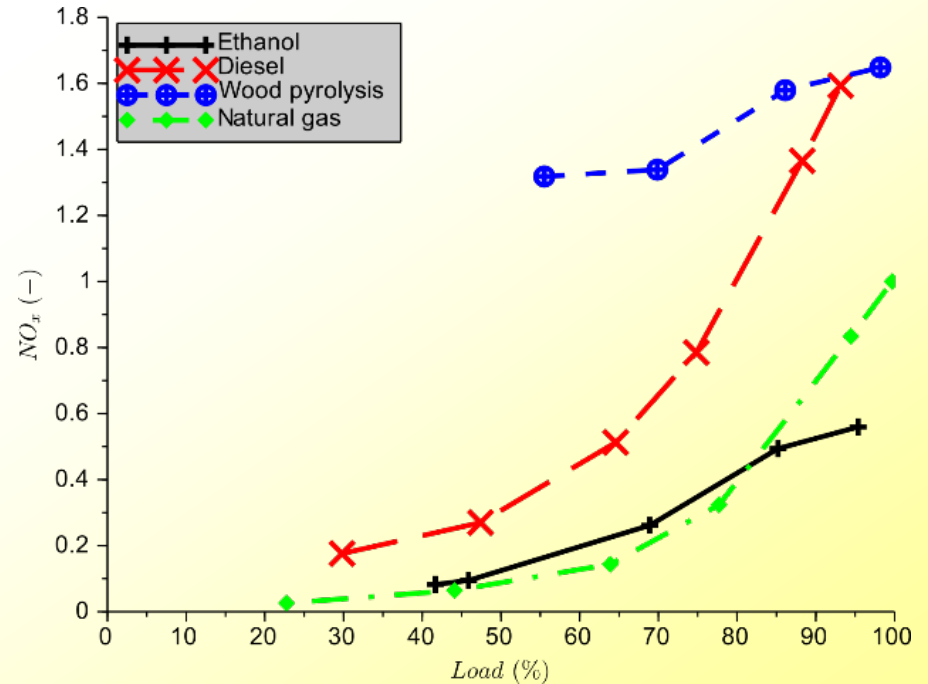
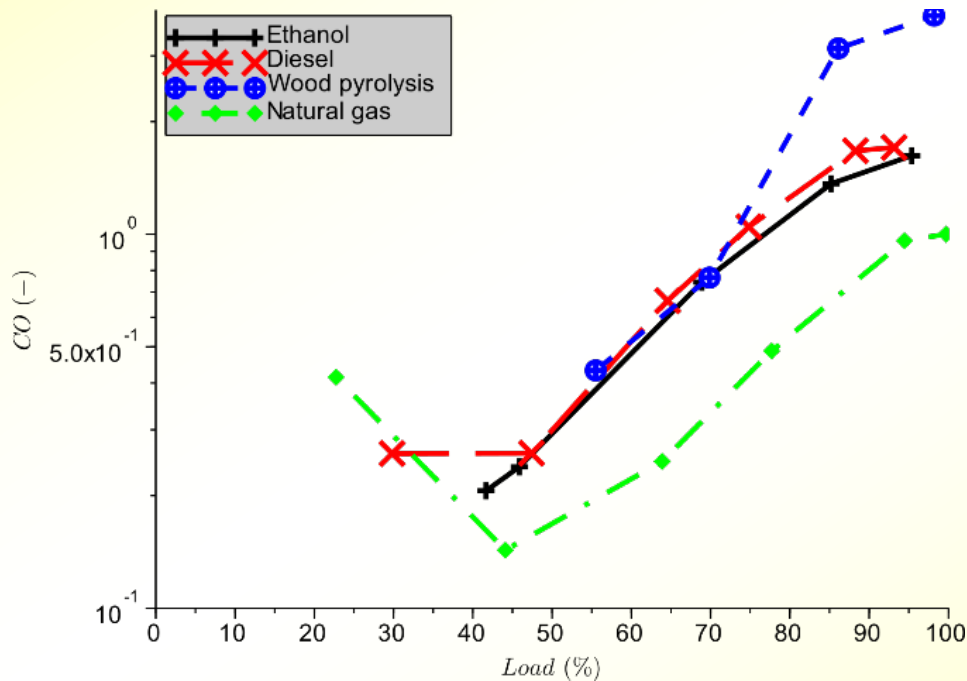
Unstable operation with poor atomization (non-suitable nozzle)



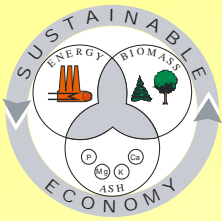
Stable operation with new nozzle

Efficient combustion of pyrolysis oil in a gas turbine combustor

- Efficient combustion of wood pyrolysis oil has been achieved in a full-scale gas turbine combustor
- Low CO levels have been reached over whole load range
- Elevated NO_x emissions due to the nitrogen content of pyrolysis oil (0.2 wt%)



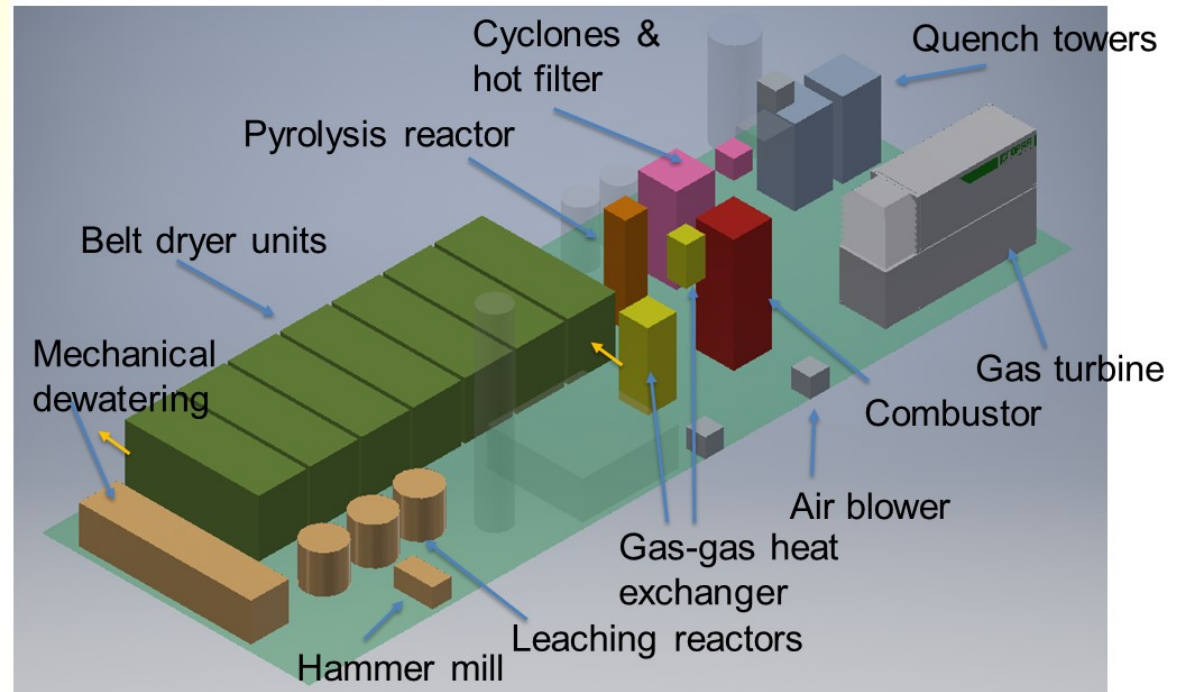
Explanation: emissions normalised

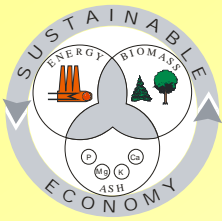


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Outlook

- The experimental work performed within the project is in its final phase
- Presently process design and process simulations regarding the overall full-scale EnCat process are on-going
- Process design is accompanied by techno-economic analyses and life-cycle assessments of the whole process chain
- The project shall be finalized in August 2020

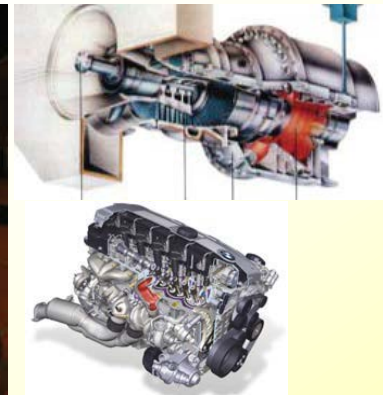




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Thank you for your attention



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