



THE USAGE OF BIOGAS IN FUEL CELL SYSTEMS

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Outline

- Biogas as renewable fuel
- Application to fuel cells
- Fuel cells requirements
- Upgrading biogas
- Future perspectives



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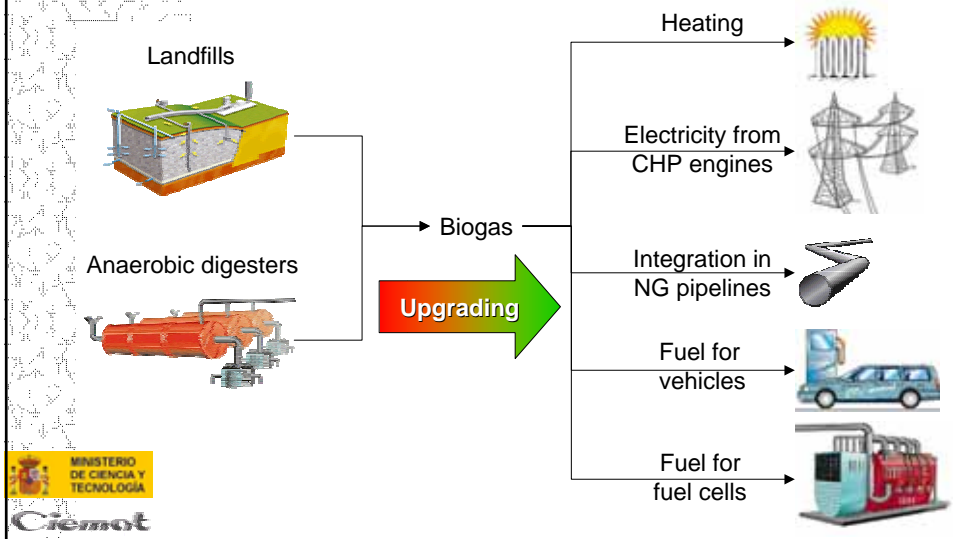
Biogas as renewable energy source

- Sustainable development: limitation of fossil fuels use
- Renewables
 - Biofuels: can be stored and transported more easily than other renewable energy sources.
 - Biogas
 - Landfill gas
 - Anaerobic digestion gas:
 - » Industrial waste water treatment
 - » Stabilisation of sewage sludge
 - » Recycling of biowaste, agricultural waste and manure as organic fertilizers

Biogas composition

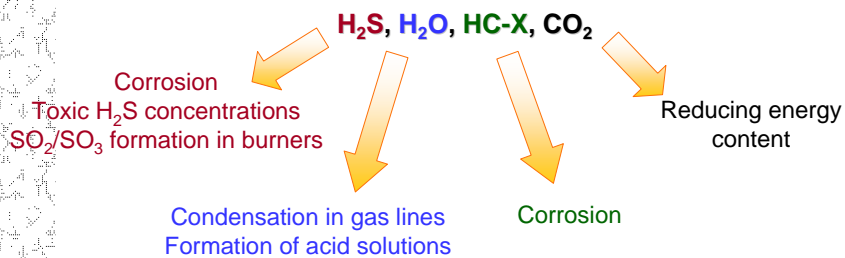
- Main components:
CH₄, CO₂, H₂S, NH₃
- Other:
N₂, O₂, H₂, CO, HC, HC-X, H₂O, siloxanes, dust particles
- Its energy content is defined by the methane concentration:
10% CH₄ ⇒ 1 kWh·m⁻³

Options for biogas utilisation

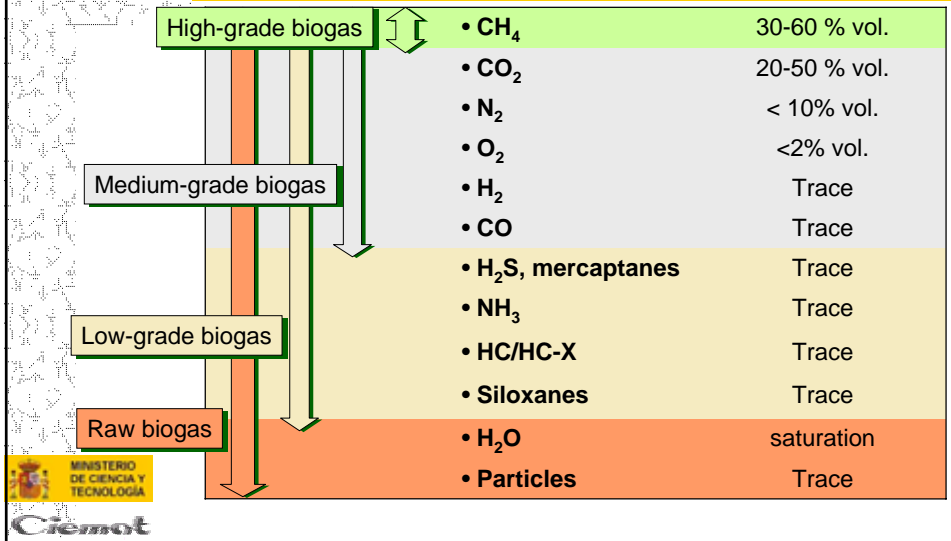


Biogas upgrading

- Depending on the final application the biogas quality have to be improved.
- Main components to remove as general rule:



Biogas components



Biogas purity grades

- Options for its final use depend on the degree of processing.
- Level of processing affects the economics of the application:

Low-grade: Heating
(end-user must be in the proximity)

Medium-grade: Heating
Gas engines
Combined heat and power (CHP)

High grade: Pipeline quality gas
Production of chemicals
Fuel for vehicles
Fuel for FC

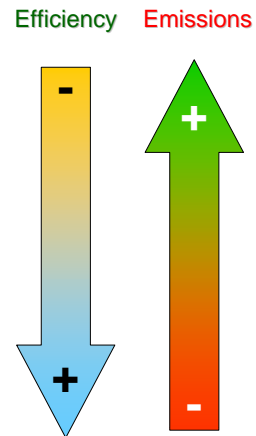
From biogas to electricity

Options:

- Gas engines and turbines
- Combined heat and power plants
- Fuel cells

Require upgrading to medium grade biogas

Require biogas upgrading & processing to obtain hydrogen



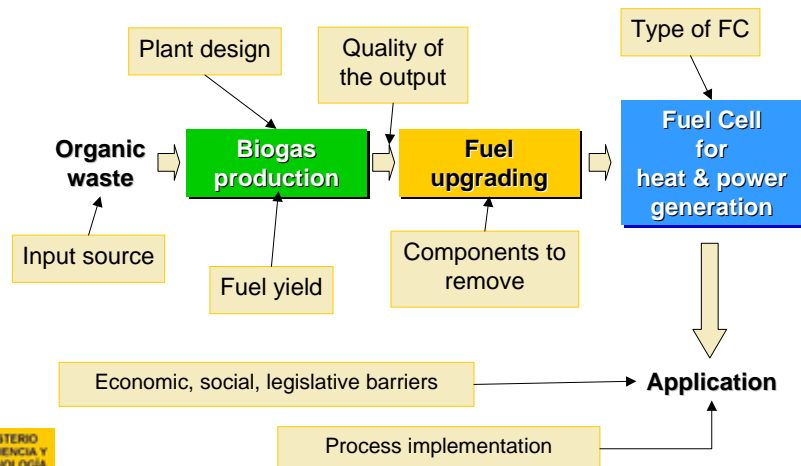
LFG and AD biogas revalorization

- Main problem associated to biogas:
 - variability of its composition:
depends on the source and varies with time
- For low CH_4 contents:
 - ignition problems in ICE:
mixtures usually vented after being burned in flares
 - can be used in FC after upgrading by using CO_2 instead of water as source of oxygen for producing H_2/CO by reforming

Fuel Cells for biogas conversion

- High temperature FCs: MCFCs, SOFCs
 - Upgrading before reforming: removal of sulfur compounds, NH_3 , halogenated HC, siloxanes
 - More tolerant to impurities
 - May operate with $\text{H}_2/\text{CO}/\text{CO}_2$ mixtures
- Low temperature FCs: PEMFCs
 - Upgrading before reforming: removal of sulfur compounds, NH_3 , halogenated HC, siloxanes
 - Fuel processing after reforming to reduce CO levels below 10 ppm.

Multidisciplinary research area



Fuel Cell feeding requirements

Component	PEMFC	PAFC	MCFC	SOFC
H ₂	Fuel	Fuel	Fuel	Fuel
CO	Poison (10 ppm)	Poison (10 ppm)	Fuel	Fuel
CH ₄	Inert	Inert	Fuel	Fuel
CO ₂ , H ₂ O	Diluent	Diluent	Recycled	Diluent
Sulfur	< 200 ppb	Poison <50 ppm H ₂ S+COS	Poison 0.1-0.5 ppm H ₂ S	Poison < 1 ppm H ₂ S
Halogens	----	Poison 4 ppm	Poison < 0.1-1.0 ppm	Poison < 1 ppm



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Fuel cell types

Fuel cell type	Electrolyte	Charge carrier	Operating temperature	Fuel	Power range/ applications	Electrical efficiency % today (target)
Alkaline FC (AFC)	KOH	OH ⁻	50-100°C	Pure H ₂	Aerospace	40-60
Proton exchange membrane FC (PEMFC)	Solid polymer (such as Nafion)	H ⁺	50-100°C	Pure H ₂ (tolerates CO ₂)	Automotive, CHP, (5-250 kW) portable	35 (45)
Phosphoric acid FC (PAFC)	Phosphoric acid	H ⁺	~ 220°C	Pure H ₂ (tolerates CO ₂ , approx. 1% CO)	CHP (200 kW)	<42
Molten carbonate FC (MCFC)	Lithium and potassium carbonate	CO ₃ ²⁻	~ 650°C	H ₂ , CO, CH ₄ , other hydrocarbons (tolerates CO ₂)	200 kW - 2 MW range, CHP and stand-alone	47 (60)
Solid oxide FC (SOFC)	Solid oxide electrolyte (yttria, zirconia)	O ²⁻	~ 1000°C	H ₂ , CO, CH ₄ , other hydrocarbons (tolerates CO ₂)	2-1000 kW range, CHP and stand-alone	47 (65)



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Biogas upgrading technologies

- Removal of moisture and particles
- Removal of trace gases:
sulfur compounds, halogen compounds, siloxanes
- Carbon dioxide stripping

Moisture removal techniques

- **Moisture separators:** reduce the gas flow velocity and allows liquid droplets to condensate in the vessel walls.
- **Mist eliminator:** filters with high surface area allows further condensation. It also allows particles removal. In combination with moisture separators removes 99.9% of the liquids.
- **Gas cooling and compression:** decreases the dew point of the gas.
- **Absorption technology:** liquids with high water affinity: glycols: EG, DEG, TEG. Require regeneration
- **Adsorbent materials:** silica gel, alumina, molecular sieves. Require regeneration.

Removal of H₂S

- **Adsorbents: activated carbon impregnated with KI** (high affinity with H₂O reduces its potential for traces removal the moisture removal step is not efficient)
- **Iron sponge, Fe₂O₃ pellets:** removal of H₂S by formation of iron sulphide (25-50°C). Adsorbent regeneration by oxidation: Fe₂O₃ + S (highly exothermic).
- **Selective solvents:**
 - Water scrubbing
 - NaOH scrubbing (Na₂S, HNaS)
 - Alkanolamine process: selective solvents mainly for H₂S and CO₂: MEA, DEA, TEA
 - Selexol scrubbing (polyethylene glycol)



2-column system for H₂S scrubbing with iron oxide

H₂S removal

- **Addition of FeCl₃ in digesters:** very effective method but needs to be complemented with another removal method to reduce H₂S level.
- **Biological desulphurisation: *thiobacillus***
Autotrophic organism consuming CO₂ and producing S and SO₄²⁻. Requires addition of some amount of O₂ (2-6%) and reduce H₂S level below 50 ppm. (Biogas in air is explosive in the range of 6 – 12 % depending on the methane content.) It is suitable for gas engines but not for FC.
- **Biological filters:** combination of water scrubbing and biological desulphurisation



Biological desulphurization unit

Siloxane removal

Organic silicon compounds are occasionally present in biogas and may affect adversely to FC performance: are widely used in cosmetics, pharmaceuticals and in anti-foaming agents in detergents

- Adsorption in a mixture of hydrocarbons: adsorbent regenerated by heating and desorption
- Cooling to -2°C and adsorption in charcoal

Halogenated hydrocarbons removal

Higher hydrocarbons and chlorinated and fluorinated compounds are commonly found in LFG: corrosive agents

- Removal by pressurized tube exchangers filled with activated carbon: PSA units
Regeneration by desorption at 200°C .



PSA unit for biogas, for H_2S , halogenated carbons, and CO_2 removal

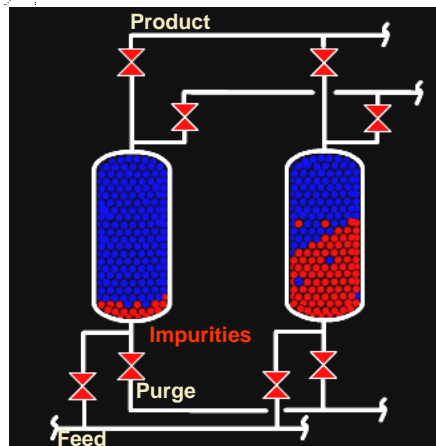
Carbon dioxide stripping

- **Solvent extraction:**
 - Water scrubbing
 - Polyethylene glycol scrubbing (Selexol)
- **Adsorption:**
 - uses a series of molecular sieves to reduce CO₂ level below 1%.
- **Membrane separation:**
 - High pressure: selective permeation membranes typically composed of cellulose acetate have been used for these purposes.
 - Gas-liquid absorption membranes: (NaOH). Operate at low pressure (1 atm) and temperature (35°C).



Renton plant
Seattle, USA
4000 m³/day

PSA systems (Pressure Swing Adsorption)

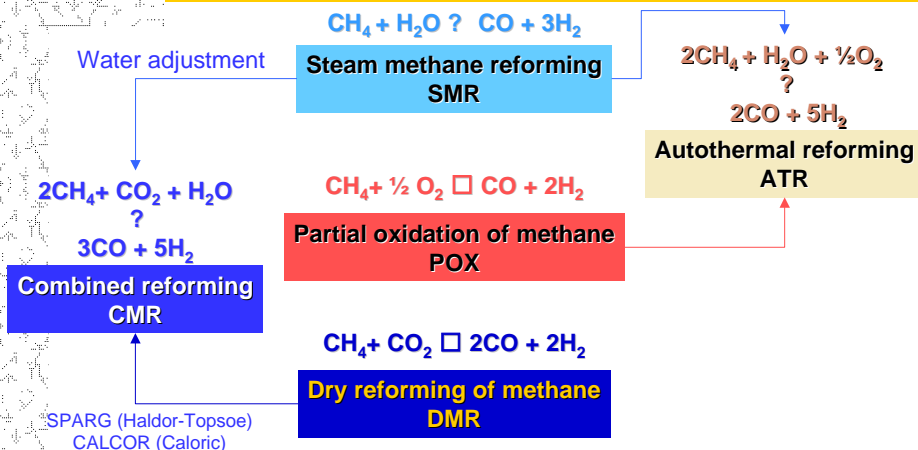


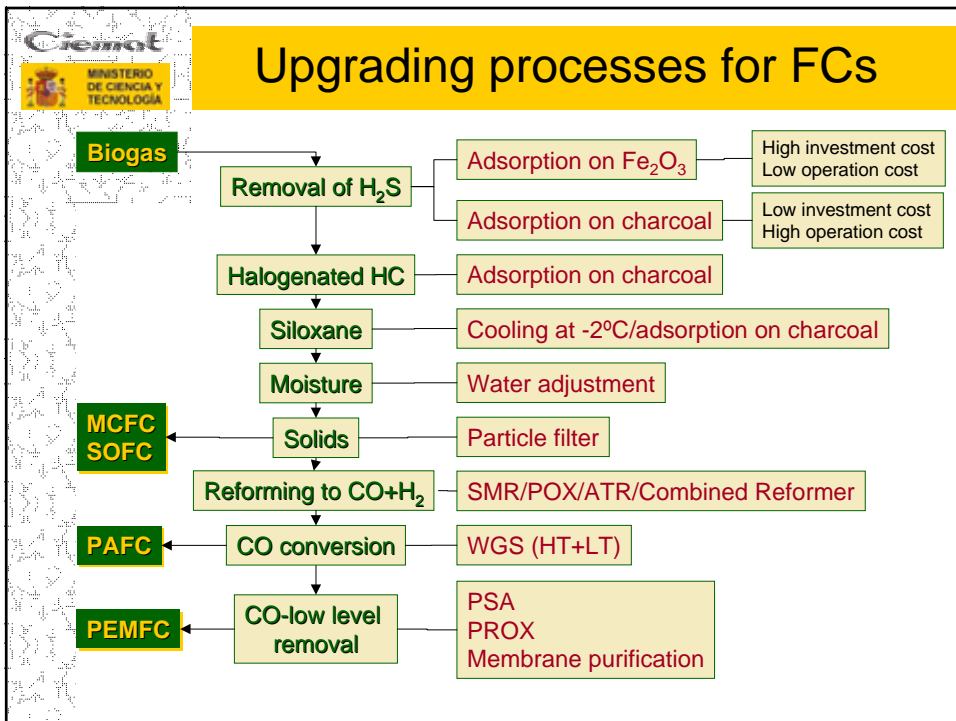
- 1 Pressure adsorption
- 2 Co-current despressurisation
- 3 Counter-current despressurisation
- 4 Purge
- 5 Pressurisation

Adsorbents in PSA systems

Adsorbent	Application: removed component
Silica gel	H ₂ O
Activated alumina	H ₂ O
Activated carbon	CO ₂ , CH ₄ , (CO)
Zeolites	CO, N ₂ , CH ₄
ZnO	H ₂ S, sulfur containing compounds

Biogas reforming







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Future perspectives


- High temperature fuel cells are more suitable for biogas use:
 - Higher tolerance to impurities
 - Higher efficiency
 - Simpler purification systems for biogas
 - Simpler reformers
 - CO₂ use for reforming: lower steam requirements



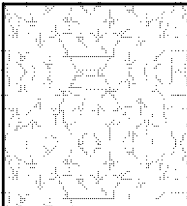
PAFC



MCFC



SOFC



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